

Hazardous Air Pollutants <i>(List Separately)</i> (1)		Stack Emission Rate (@ Rated Capacity) (2)				
		Pounds Per Hour (lb/hr) (a)	Tons per year (TPY) (b)	Concentration Micrograms Per Cubic Meter ($\mu\text{g}/\text{m}^3$) (c)	Other (Units) (d)	Basis (e)
Lead	uncontrolled potential	3.24E-3	1.42E-2			Fuel Analysis
	proposed actual	3.24E-3	6.74E-4	2.70		Fuel Analysis
	maximum allowable			10		RCSA 22a-174-29
Manganese	uncontrolled potential	3.70E-2	1.62E-1			Fuel Analysis
	proposed actual	3.70E-2	7.70E-3	30.83		Fuel Analysis
	maximum allowable			69		RCSA 22a-174-29
Mercury	uncontrolled potential	2.77E-4	1.21E-3			Fuel Analysis
	proposed actual	2.77E-4	5.78E-5	0.23		Fuel Analysis
	maximum allowable			3		RCSA 22a-174-29
Nickel	uncontrolled potential	1.06E-3	4.64E-3			Fuel Analysis
	proposed actual	1.06E-3	2.21E-4	0.89		Fuel Analysis
	maximum allowable			17		RCSA 22a-174-29
Selenium	uncontrolled potential	5.78E-3	2.53E-2			Fuel Analysis
	proposed actual	5.78E-3	1.70E-3	4.82		Fuel Analysis
	maximum allowable			14		RCSA 22a-174-29

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Sulfuric Acid	uncontrolled potential	3.97E-2	1.74E-1			Fuel Analysis
	proposed actual	3.97E-2	1.43E-2	33.99		Fuel Analysis
	maximum allowable			69		RCSA 22a-174-29
	uncontrolled potential					
	proposed actual					
	maximum allowable					
	uncontrolled potential					
	proposed actual					
	maximum allowable					
	uncontrolled potential					
	proposed actual					
	maximum allowable					
	uncontrolled potential					
	proposed actual					
	maximum allowable					

Section IV: Fugitive Emission Information for Listed Pollutants

Pollutant	Emission Rate (@ Rated Capacity) (1)			
	Pounds Per Hour (lb/hr) (a)	Tons Per Year (TPY) (b)	Other Units (c)	Basis (d)
Carbon Monoxide (CO)	uncontrolled potential			
	proposed actual			
Volatile Organic Compounds (VOC)	uncontrolled potential			
	proposed actual			
Exempted Volatile Organic Compounds	uncontrolled potential			
	proposed actual			
Hydrocarbons	uncontrolled potential			
	proposed actual			
Nitrogen Oxides (NOx)	uncontrolled potential			
	proposed actual			
Sulfur Oxides (SOx)	uncontrolled potential			
	proposed actual			
Particulate Matter (TSP)	uncontrolled potential			
	proposed actual			
Particulate Matter <- 10 Micrometers (PM ₁₀)	uncontrolled potential			
	proposed actual			
Lead (Pb)	uncontrolled potential			
	proposed actual			
1e. Assumptions:				

Section V: Fugitive Emission Information for Hazardous Air Pollutants

Hazardous Air Pollutants <i>(List Separately)</i> (1)	Emission Rate (@ Rated Capacity) (2)				
	Pounds Per Hour (lb/hr) (a)	Tons per year (TPY) (b)	Concentration Micrograms Per Cubic Meter ($\mu\text{g}/\text{m}^3$) (c)	Other (Units) (d)	Basis (e)
	uncontrolled potential				
	proposed actual				
	maximum allowable				
	uncontrolled potential				
	proposed actual				
	maximum allowable				
	uncontrolled potential				
	proposed actual				
	maximum allowable				
	uncontrolled potential				
	proposed actual				
	maximum allowable				
	uncontrolled potential				
	proposed actual				
	maximum allowable				

ATTACHMENT E

UNIT EMISSIONS CALCULATIONS

Criteria Pollutant Emission Calculations

For gaseous fuel firing at 25 ppmvd at 15% O₂, GE provided TM2500 operating data for three full-load operating scenarios: operation at 0, 50, and 100°F ambient temperatures (see Attachment E-1 for the GE data sheets). For liquid fuel firing at 42 ppmvd at 15% O₂, GE provided TM2500 operating data for six full-load operating scenarios: operation at 0, 50, 100 (three cases provided: over-fire; expected; and guaranteed), and 90°F ambient temperature (see Attachments E-2 and E-3 for the GE data sheets).

The NO_x, CO, and HC emissions are based on emission factors provided by AP-42 for natural gas and the turbine vendor for oil firing.

The NO_x, CO, and HC (and thus VOC) emissions are calculated as follows

$$\text{Mass Emission Rate (lb/hr)} = \frac{\text{ppmvd@15\% O}_2}{10^6} \times \frac{\text{lb/hr Exhaust}}{\text{Exhaust MW}} \times \text{vol.\% Water} \times \text{Pollutant MW} \times \frac{20.9 - \% \text{ O}_2}{20.9 - 15}$$

Using the following molecular weights:

$$\begin{aligned} NO_x &= 46 \\ CO &= 28 \\ VOC &= 16 \end{aligned}$$

The SO₂ emission factor is derived by mass balance using a conservative assumption of 0.8 gr/100 ft³ of sulfur in the gaseous fuel and 0.0015% (or 15 ppmw) sulfur of the liquid fuel. It is conservatively assumed that all the sulfur in the fuel is converted to SO₂. The SO₂ emissions are calculated as follows:

$$\text{For natural gas: lb/hr } SO_2 = \frac{gr S}{100 \text{ scf gas}} \times \frac{1 \text{ lb}}{7000 \text{ gr}} \times \frac{1 \text{ scf gas}}{1020 \text{ Btu}} \times \frac{Btu}{hr} (\text{Heat Input})$$

$$\text{For oil firing: lb/hr } SO_2 = \frac{\% S}{100} \times \frac{lb \text{ fuel}}{hr} \times \frac{2 \text{ mol } SO_2}{1 \text{ mol S}}$$

Finally, an AP-42 emission factor of 1.2×10^{-2} lb/MMBtu for liquid fuel firing and 6.6×10^{-3} lb/MMBtu for gaseous fuel firing are used to derive the PM emissions. It is conservatively assumed that all PM is PM10.

A detailed spreadsheet with the calculations for both criteria and non-criteria pollutants is presented in Attachment E-4.

Non-Criteria Pollutant Emission Calculations

AP-42, Section 3.1 emissions factors were used for the following HAPs: 1,3 butadiene, acetaldehyde, benzene, ethylbenzene, naphthalene, PAH (total), propylene oxide, toluene, xylenes, chromium, mercury, nickel, and selenium. The benzene soluble PAH emission factor was calculated as the total PAH emission factor for a combustion turbine using the speciation of PAH (from AP-42, Table 1.3.9 for liquid fuel and Table 1.4.3 for gaseous fuel by the fraction of PAH that is benzene soluble (see Attachment E-5 for gaseous fuel operation and Attachment E-6 for liquid fuel operation). Similarly, the coal tar pitch volatile ("CTPV") emission factor was calculated as the total PAH emission factor for a combustion turbine using the speciation of PAH by the fraction of PAH that are CTPVs (see Attachment E-5 for gaseous fuel operation and Attachment E-6 for liquid fuel operation).

The formaldehyde emission factor was derived from the background document for AP-42, Section 3.1, which includes the emissions from a LM2500 unit with water injection. The emission factor used was for natural gas firing and it was conservatively assumed that the same factor is for oil.

A fuel analysis of ultra-low sulfur distillate fuel that was used for the recently permitted South Norwalk Electric Works GE TM2500 gas turbine (Permit No. 0140 issued in June, 2003) was used to derive the emission factors for arsenic, beryllium, cadmium, lead, and manganese (see Attachment E-7).

The sulfuric acid (H_2SO_4) emission factor was developed from a CT DEP memo dated November 27, 1987.

For liquid fuel, sulfuric acid is calculated as:

$$H_2SO_4 (\text{lb}/1000 \text{ gals fuel fired}) = 2 \times \% \text{ sulfur} \times 1.225 (\text{lb}/1000 \text{ gal})$$

where the % sulfur is 0.0015.

For gaseous fuel, sulfuric acid is calculated as:

$$H_2SO_4 (\text{lb}/\text{MMBtu}) = 0.8 \text{ gr}/100 \text{ cu. ft.} \times 1 \text{ cu. ft}/1,020 \text{ Btu} \times 1 \text{ lb}/7000 \text{ gr. S} \times 1 \times 10^6 \text{ Btu}/\text{MMBtu} \times 0.05 \text{ lbs S}/1 \text{ lb S} \times 98 \text{ lb-Mol } H_2SO_4/32 \text{ lb-mol S}$$

Uncontrolled Potential and Proposed Actual

The maximum uncontrolled potential emissions are the rate of emissions from the unit in lbs/hr (see Table A-2 for criteria pollutants and Table A-4 for non-criteria pollutants) operating at a maximum rated capacity of 8,760 hours per year. The uncontrolled potential and proposed actual hourly emissions in lbs/hour are identical. The annual uncontrolled potential emissions are calculated as the uncontrolled hourly potential times 8,760 hours per year. The maximum proposed actual emissions take into account the fuel use restrictions. Thus, the per unit emissions are calculated as follows:

Annual Uncontrolled Potential (tpy) =

$$\text{Uncontrolled Potential (lb/hr)} \times 8,760 \text{ (hrs/yr)} / 2,000 \text{ (lbs/ton)}$$

Proposed Actual (tpy) =

$$\text{Proposed Actual (lb/hr)} \times [(540,905,000 \text{ scf}/251,000 \text{ scf/hr}) \text{ for gaseous fuel}; \\ (2,249,100 \text{ gals}/1,800 \text{ gals/hr}) \text{ for liquid fuel}] \text{ (hrs/yr)}/2,000 \\ (\text{lbs/ton})$$

The uncontrolled potential and proposed actual are the maximum emission rates for gaseous and liquid fuel firing over all scenarios analyzed.

MASC Analysis

The maximum allowable stack concentration ("MASC") has been calculated for each HAP that will be emitted and that is listed in Tables 29-1, 29-2, or 29-3 of §22a-174-29. The methodology described in §22a-174-29 was used to calculate the MASC in lb/hr. To compute the concentration in $\mu\text{g}/\text{m}^3$, the following formula was used:

$$\text{Concentration } (\mu\text{g}/\text{m}^3) = \text{emission rate (lb/hr)} \times (1/\text{minimum actual flow rate in ft}^3/\text{min}) \times \\ (453.59 \times 10^6 \mu\text{g/lb}) \times (1 \text{ hr}/60 \text{ min}) \times (35.314 \text{ ft}^3/\text{m}^3)$$

The predicted stack concentrations are compared with the 8-hr HLV (ground level) limits as per § 22a-174-29 in Attachments E-8 through E-10 for units 1 through 3 firing gaseous fuel and E-11 through E-13 firing liquid fuel. For each HAP, the predicted stack concentration is less than the MASC.

ATTACHMENT E-1:
General Electric LM2500 Emissions Data for Gaseous Fuel Firing

GE AERO ENERGY PRODUCTS/GE LM2500-Standard Estimated Average Engine Performance NOT FOR GUARANTEE NAT GAS
 GENERATOR: 170R, 60 Hz, 13.8 kV, 0.9 PF EFF: 7514 CAP: 7343 md: 2/001 1:58:17 PM GE166A PEpp 1.0-1
 TM2500 Gas 25ppm

% LOAD	100%	100%	100%
CASE #	100	110	120
AMBIENT			
DB, °F	0.0	50.0	100.0
WB, °F	-1.2	43.6	88.9
RH, %	60.0	60.0	60.0
ALT, FT	200	200	200
ENGINE INLET			
TEMP, °F	0.0	50.0	100.0
RH, %	60.0	60.0	60.0
CONDITIONING	NONE	NONE	NONE
TONS or kBtu	0	0	0
KW, GENTERM	23548	23393	19720
Btu/KW-hr, LHV	9752	9888	10122
FUEL			
MMBtu/hr, LHV	229.6	231.3	199.6
lb/hr	11,081	11,162	9,632
NOZZLE WATER			
lb/hr	11772	12644	8910
*F	100	100	100
NOZZLE STEAM			
lb/hr	0	0	0
*F	0	0	0
COP STEAM			
lb/hr	0	0	0
*F	0	0	0
INLET LOSS, inH2O	4.0	4.0	4.0
EXHAUST LOSS, inH2O	16	16	16
HP COMP, rpm	3600	3600	3600
LP COMP, rpm	9329	9613	9409
COMP DISCH, psia	280	272.5	241.1
COMP DISCH, °F	768	860	877
T48, °R	1822	1925	1925
EXHAUST PARAMETERS			
*F	868	958	990
lb/sec	164.8	158.2	139
lb/hr	593280	562320	500400
Cp Btu/lb-R	0.275	0.2806	0.2851
EMISSIONS (NOT FOR USE IN ENVIRONMENTAL PERMITS; Ref @ 15% O2)			
NOx, ppmvd	25	25	25
NOx, lb/hr	23	23	20
CO, ppmvd	99	53	20
CO, lb/hr	58	30	10
HC, ppmvd	31	12	3
HC, lb/hr	10	4	1
EXH WEIGHT % WET (NOT FOR USE IN ENVIRONMENTAL PERMITS)			
AR	1.2377	1.2279	1.2098
N2	72.6082	72.0333	70.9710
O2	15.0879	14.4551	14.3553
CO2	5.0385	5.3631	5.2086
H2O	6.0130	6.9118	8.2505
SO2	0.0000	0.0000	0.0000
CO	0.0094	0.0053	0.0018
HC	0.0017	0.0007	0.0002
NOx	0.0027	0.0028	0.0028
EXH MOLE % DRY (NOT FOR USE IN ENVIRONMENTAL PERMITS)			
AR	0.9654	0.9578	0.9673
N2	80.7982	80.9612	80.9178
O2	14.6211	14.2238	14.3294
CO2	3.5680	3.8370	3.7802
H2O	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000
CO	0.0104	0.0050	0.0022
HC	0.0032	0.0014	0.0004
NOx	0.0026	0.0028	0.0028
EXH MOLE % WET (NOT FOR USE IN ENVIRONMENTAL PERMITS)			
AR	0.8744	0.8636	0.8438
N2	73.1506	72.2351	70.5916
O2	13.3080	12.6908	12.5008
CO2	3.2319	3.4234	3.2978
H2O	9.4203	10.7782	12.7613
SO2	0.0000	0.0000	0.0000
CO	0.0085	0.0053	0.0019
EXHAUST MW	26.2200	26.0900	27.8600
HC	0.0029	0.0012	0.0003
NOx	0.0024	0.0025	0.0024

ATTACHMENT E-2:
General Electric LM2500 Emissions Data for Liquid Fuel Firing

GE AERO ENERGY PRODUCTS/GE LM2500-Standard Estimated Average Engine Performance NOT FOR GUARANTEE UQ FBn:0.015 Sulfur:0.1
 GENERATOR: 170R, 60 Hz, 13.8 kV, 0.9 PF EFF: 7514 CAP: 7343 JG 2/12/01 2:56:54 PM GE168A PE:pip 1.0-1
 TM2500 Distillate Fuel Oil 42ppm

% LOAD	100%	100%	100%
CASE #	100	110	120
AMBIENT			
DB, °F	0.0	50.0	100.0
WB, °F	-12	43.6	86.9
RH, %	60.0	60.0	60.0
ALT, FT	200	200	200
ENGINE INLET			
TEMP, °F	0.0	50.0	100.0
RH, %	60.0	60.0	60.0
CONDITIONING	NONE	NONE	NONE
TONS or kBtu	0	0	0
KW, GEN TERM	23499	23131	19001
Btu/KWhr, LHV	9842	9991	10300
FUEL			
MMBtu/hr, LHV	231.3	231.1	195.7
lb/hr	12,569	12,560	10,636
NOZZLE WATER			
lb/hr	13226	14129	9527
*F	100	100	100
NOZZLE STEAM			
lb/hr	0	0	0
*F	0	0	0
CDP STEAM			
lb/hr	0	0	0
*F	0	0	0
INLET LOSS, inH2O	4.0	4.0	4.0
EXHAUST LOSS, inH2O	16	16	16
HP COMP, rpm	3600	3600	3600
LP COMP, rpm	9289	9525	9353
COMP DISCH, psia	280	271.1	236
COMP DISCH, °F	765	852	868
T48, °R	1829	1926	1925
EXHAUST PARAMETERS			
*F	875	960	996
lb/sec	165.5	155.5	137.1
lb/hr	595600	563400	493560
Cp Btu/lb-R	0.273	0.2782	0.2626
EMISSIONS (NOT FOR USE IN ENVIRONMENTAL PERMITS, Ref @ 15% O2)			
NOx, ppmvd	42	42	42
NOx, lb/hr	40	40	34
CO, ppmvd	91	44	21
CO, lb/hr	53	25	10
HC, ppmvd	8	4	2
HC, lb/hr	2	1	1
EXH WGHT % WET (NOT FOR USE IN ENVIRONMENTAL PERMITS)			
AR	1.2315	1.2214	1.2350
N2	72.2093	71.6142	70.6521
O2	15.0556	14.4684	14.4207
CO2	6.7398	7.1277	6.6953
H2O	4.7456	5.5543	6.8157
SO2	0.0042	0.0045	0.0043
CO	0.0089	0.0045	0.0021
HC	0.0004	0.0002	0.0001
NOx	0.0046	0.0049	0.0047
EXH MOLE % DRY (NOT FOR USE IN ENVIRONMENTAL PERMITS)			
AR	0.6537	0.6560	0.6546
N2	79.7372	79.8502	79.8151
O2	14.5552	14.1237	14.2226
CO2	4.7375	5.0589	4.9584
H2O	0.0000	0.0000	0.0000
SO2	0.0019	0.0020	0.0019
CO	0.0098	0.0050	0.0024
HC	0.0009	0.0005	0.0002
NOx	0.0045	0.0048	0.0047
EXH MOLE % WET (NOT FOR USE IN ENVIRONMENTAL PERMITS)			
AR	0.6818	0.6711	0.6825
N2	73.7291	72.8358	71.2805
O2	13.4585	12.8830	12.7375
CO2	4.3805	4.6145	4.4282
H2O	7.5350	8.7845	10.6929
SO2	0.0019	0.0020	0.0019
CO	0.0091	0.0046	0.0021
EXHAUST MW	28.6000	28.4600	28.2600
HC	0.0008	0.0004	0.0002
NOx	0.0042	0.0044	0.0042

Btu/b, LHV

ATTACHMENT E-3:
General Electric LM2500 Emissions Data for Liquid Fuel Firing at 90°F

NOT FOR GUARANTEE

GE AERO ENERGY PRODUCTS/GE LM2500-Standard Estimated Average Engine Performance LIQ FBN:0.015 Sulfur:0.003
 GENERATOR: 167ER, 60 Hz, 13.8 kV, 1.0 PF EFF: 10807 CAP: 10805 SS 4/5/2002 11:51:31 AM GE166A PE.pip 2.0-0

	Over-fire	Expected	Guaranteed
CASE #	100	101	102
AMBIENT			
DB, °F	90.0	90.0	90.0
WB, °F	78.2	78.2	78.2
RH, %	60.0	60.0	60.0
ALT, FT	10	10	10
ENGINE INLET			
TEMP, °F	90.0	90.0	90.0
RH, %	60.0	60.0	60.0
CONDITIONING	NONE	NONE	NONE
TONS or kBtu	0	0	0
KW GEN TERM	23298	22123	21009
MMBtu/hr,LHV	9056	10653	10590
FUEL			
MMBtu/hr, LHV	233.4	221.5	211.1
lb/hr	12,684	12,040	11,474
NOZZLE WATER			
lb/hr	13567	12331	11356
°F	100	100	100
NOZZLE STEAM			
lb/hr	0	0	0
°F	0	0	0
CDP STEAM			
lb/hr	0	0	0
°F	0	0	0
INLET LOSS,inH2O	4.0	4.0	4.0
EXHAUST LOSS,inH2O	6	6	6
HP COMP, rpm	3600	3600	3600
LP COMP, rpm	9775	9555	9403
COMP DISCH, psia	266.1	258.6	251.1
COMP DISCH, °F	919	894	875
T48, °R	2010	1970	1938
EXHAUST PARAMETERS			
°F	1030	1004	985
lb/sec	150.3	147.9	145.1
lb/hr	541080	532440	522360

Cp Btu/lb-R	0.2844	0.2827	0.2814
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EMISSIONS (NOT FOR USE IN ENVIRONMENTAL PERMITS, Ref @ 15% O₂)

NOx, ppmvd	42	42	42
NOx, lb/hr	40	38	37
CO, ppmvd	16	20	24
CO, lb/hr	9	11	13
HC, ppmvd	2	2	2
HC, lb/hr	1	1	1

EXH WGHT % WET (NOT FOR USE IN ENVIRONMENTAL PERMITS)

AR	1.2036	1.2070	1.2097
N ₂	70.5706	70.7732	70.9262
O ₂	13.7592	14.0977	14.3610
CO ₂	7.5018	7.2394	7.0340
H ₂ O	6.9578	6.6754	6.4618
SO ₂	0.0000	0.0000	0.0000
CO	0.0017	0.0021	0.0024
HC	0.0001	0.0001	0.0001
NO _x	0.0051	0.0050	0.0048

EXH MOLE % DRY (NOT FOR USE IN ENVIRONMENTAL PERMITS)

AR	0.9565	0.9556	0.9549
N ₂	79.9737	79.9003	79.8434
O ₂	13.6511	13.9341	14.1537
CO ₂	5.4116	5.2026	5.0404
H ₂ O	0.0000	0.0000	0.0000
SO ₂	0.0000	0.0000	0.0000
CO	0.0020	0.0024	0.0027
HC	0.0002	0.0002	0.0003
NO _x	0.0052	0.0050	0.0048

EXH MOLE % WET (NOT FOR USE IN ENVIRONMENTAL PERMITS)

AR	0.852	0.8554	0.8579
N ₂	71.2389	71.5189	71.7296
O ₂	12.1601	12.4724	12.7154
CO ₂	4.8205	4.6568	4.5282
H ₂ O	10.9221	10.4899	10.1622
SO ₂	0.0000	0.0000	0.0000
CO	0.0018	0.0022	0.0024
EXHAUST MW	28.2800	28.3100	28.3300
HC	0.0002	0.0002	0.0002
NO _x	0.0046	0.0044	0.0043

Btu/lb, LHV	18400
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Attachment E-4. Detailed Emissions Calculations

Input Data: 100% Load
25 ppm Gaseous Fuel / 42 ppm Liquid Fuel NO_x

Stack Data:

Stack Dimensions: 8.21875 feet x 8.234375 feet
Stack Area: 67.68 Sq. Ft.
Site Elevation: 10 feet (above MSL)

Fuel Data:

Natural Gas
Heat Content: 19,000 Btu/lb (LHV)
HHV/LHV Ratio: 1.1051 (dimensionless)
Sulfur Content: 0.80 gr/100 ft³

Fuel Oil

Heat Content: 18,400 Btu/lb (LHV)
Fuel Density: 7.1 lb/gal
HHV/LHV Ratio: 1.067 (dimensionless)
Sulfur Content: 0.0015 %
Vendor Reference Nitrogen: 0 %
Fuel Nitrogen Content: 0.05 %

General Title Information:

Project Number: 61514
Client or Company Name: Waterside Power, LLC
Date of Report: 09/04/03 Updated 10/22/07
Turbine Mfg: GE
Turbine Model #: LM2500
40690

Fuel cont.	Natural Gas 100%			Oil 100%		
	Over-Fine	Expected	Guaranteed	Over-Fine	Expected	Guaranteed
Ambient Temperature, F:	0	50	100	90	90	100
Engine Inlet Temperature:	0	50	100	90	90	100
Conditioning:	NONE	NONE	NONE	NONE	NONE	NONE
Output, kW:	23,548	23,393	19,720	23,298	22,123	21,009
Heat Rate (HHV), Btu/kWh:	9,750	9,888	10,122	10,689	10,683	10,721
Fuel Consumption, lb/hr:	11,081	11,162	9,632	12,685	12,038	11,473
Heat Cons. (LHV), MM Btu/hr:	229.6	231.3	199.6	233.4	221.5	211.1
Heat Cons. (HHV), MM Btu/hr:	253.72	255.60	220.57	249.04	236.34	225.24
Nozzle Water Inj. Rate (lb/hr):	11,772	12,644	8,910	13,667	27,536	27,538
Water/fuel injection ratio:	1.06	1.13	0.93	1.07	2.29	2.40
Spin Cycle Water (lb/hr):	N/A	N/A	N/A	N/A	N/A	N/A
Exhaust Flow, lb/hr:	593,260	562,320	500,400	541,080	532,440	522,360
Exhaust Flow, acfm:	339,696	345,274	316,782	346,883	335,031	324,192
Exhaust Temp, F:	868	958	999	1030	1004	985
Stack Exit Temp, F:	868	958	999	1030	1004	984
Stack Exit Flow, acfm:	339,696	345,274	316,782	346,883	335,031	324,192
Exit Velocity, fps:	83.66	85.03	78.01	85.43	82.51	79.84
Exhaust Composition						
Nitrogen:	mwe= 28	73.15	72.24	70.59	71.2389	71.5189
Argon:	mwe= 40	0.87	0.86	0.84	0.8552	0.8554
Oxygen:	mwe= 32	13.31	12.69	12.50	12.1601	12.4724
Carbon Dioxide:	mwe= 44	3.23	3.42	3.30	4.8205	4.6568
Water:	mwe= 18	9.42	10.78	12.76	10.9221	10.4899
Exhaust Weight, lb/Mole:						
Thermal NOx, ppmv @ 15% O2:						
Thermal NOx, lb/hr:	25	25	25	GE	42	42
CO, ppmv(15%O2):	23	23	20.1	40.5	38.4	36.6
CO, lb/hr:	99	53	20	GE	16	20
HC, ppmv @ 15%O2:	55.5	30	9.8	9.4	11.1	12.7
HC, ppmv @ 15%O2:	31	12	3	2	2	2
HCl, lb/hr:	9.90	3.90	0.80	0.7	0.6	0.6
VOC, ppmv @ 15%O2:	9.0	9.0	AP-42	2	2	2
VOC, lb/hr:	2.90	2.90	2.50	0.70	0.60	0.50
Sulfur, lb/hr:	0.3	0.3	0.2	Mass Balance	0.2	0.2
SO2, lb/hr:	0.5	0.5	0.5	0.38	0.36	0.34
SO2, ppmv:	0.44	0.47	0.47	0.3	0.3	0.3
TSP, lb/hr:	1.5	1.5	1.3	2.8	2.7	2.5
PM-10, lb/hr:	1.5	1.5	1.3	AP-42	2.8	2.8

Fuel cont.	Natural Gas 100%			Oil 100%		
	Over-Fine	Expected	Guaranteed	Over-Fine	Expected	Guaranteed
Ambient Temperature, F:	0	50	100	90	90	100
Engine Inlet Temperature:	0	50	100	90	90	100
Conditioning:	NONE	NONE	NONE	NONE	NONE	NONE
Output, kW:	23,548	23,393	19,720	23,298	22,123	21,009
Heat Rate (HHV), Btu/kWh:	9,750	9,888	10,122	10,689	10,683	10,721
Fuel Consumption, lb/hr:	11,081	11,162	9,632	12,685	12,038	11,473
Heat Cons. (LHV), MM Btu/hr:	229.6	231.3	199.6	233.4	221.5	211.1
Heat Cons. (HHV), MM Btu/hr:	253.72	255.60	220.57	249.04	236.34	225.24
Nozzle Water Inj. Rate (lb/hr):	11,772	12,644	8,910	13,667	27,536	27,538
Water/fuel injection ratio:	1.06	1.13	0.93	1.07	2.29	2.40
Spin Cycle Water (lb/hr):	N/A	N/A	N/A	N/A	N/A	N/A
Exhaust Flow, lb/hr:	593,260	562,320	500,400	541,080	532,440	522,360
Exhaust Flow, acfm:	339,696	345,274	316,782	346,883	335,031	324,192
Exhaust Temp, F:	868	958	999	1030	1004	985
Stack Exit Temp, F:	868	958	999	1030	1004	984
Stack Exit Flow, acfm:	339,696	345,274	316,782	346,883	335,031	324,192
Exit Velocity, fps:	83.66	85.03	78.01	85.43	82.51	79.84
Exhaust Weight, lb/Mole:						
Thermal NOx, ppmv @ 15% O2:						
Thermal NOx, lb/hr:	25	25	25	GE	42	42
CO, ppmv(15%O2):	23	23	20.1	40.5	38.4	36.6
CO, lb/hr:	99	53	20	GE	16	20
HC, ppmv @ 15%O2:	55.5	30	9.8	9.4	11.1	12.7
HC, ppmv @ 15%O2:	31	12	3	2	2	2
HCl, lb/hr:	9.90	3.90	0.80	0.7	0.6	0.6
VOC, ppmv @ 15%O2:	9.0	9.0	AP-42	2	2	2
VOC, lb/hr:	2.90	2.90	2.50	0.70	0.60	0.50
Sulfur, lb/hr:	0.3	0.3	0.2	Mass Balance	0.2	0.2
SO2, lb/hr:	0.5	0.5	0.5	0.38	0.36	0.34
SO2, ppmv:	0.44	0.47	0.47	0.3	0.3	0.3
TSP, lb/hr:	1.5	1.5	1.3	2.8	2.7	2.5
PM-10, lb/hr:	1.5	1.5	1.3	AP-42	2.8	2.8

Fuel cont.	Natural Gas 100%			Oil 100%		
	Over-Fine	Expected	Guaranteed	Over-Fine	Expected	Guaranteed
Ambient Temperature, F:	0	50	100	90	90	100
Engine Inlet Temperature:	0	50	100	90	90	100
Conditioning:	NONE	NONE	NONE	NONE	NONE	NONE
Output, kW:	23,548	23,393	19,720	23,298	22,123	21,009
Heat Rate (HHV), Btu/kWh:	9,750	9,888	10,122	10,689	10,683	10,721
Fuel Consumption, lb/hr:	11,081	11,162	9,632	12,685	12,038	11,473
Heat Cons. (LHV), MM Btu/hr:	229.6	231.3	199.6	233.4	221.5	211.1
Heat Cons. (HHV), MM Btu/hr:	253.72	255.60	220.57	249.04	236.34	225.24
Nozzle Water Inj. Rate (lb/hr):	11,772	12,644	8,910	13,667	27,536	27,538
Water/fuel injection ratio:	1.06	1.13	0.93	1.07	2.29	2.40
Spin Cycle Water (lb/hr):	N/A	N/A	N/A	N/A	N/A	N/A
Exhaust Flow, lb/hr:	593,260	562,320	500,400	541,080	532,440	522,360
Exhaust Flow, acfm:	339,696	345,274	316,782	346,883	335,031	324,192
Exhaust Temp, F:	868	958	999	1030	1004	985
Stack Exit Temp, F:	868	958	999	1030	1004	984
Stack Exit Flow, acfm:	339,696	345,274	316,782	346,883	335,031	324,192
Exit Velocity, fps:	83.66	85.03	78.01	85.43	82.51	79.84
Exhaust Weight, lb/Mole:						
Thermal NOx, ppmv @ 15% O2:						
Thermal NOx, lb/hr:	25	25	25	GE	42	42
CO, ppmv(15%O2):	23	23	20.1	40.5	38.4	36.6
CO, lb/hr:	99	53	20	GE	16	20
HC, ppmv @ 15%O2:	55.5	30	9.8	9.4	11.1	12.7
HC, ppmv @ 15%O2:	31	12	3	2	2	2
HCl, lb/hr:	9.90	3.90	0.80	0.7	0.6	0.6
VOC, ppmv @ 15%O2:	9.0	9.0	AP-42	2	2	2
VOC, lb/hr:	2.90	2.90	2.50	0.70	0.60	0.50
Sulfur, lb/hr:	0.3	0.3	0.2	Mass Balance	0.2	0.2
SO2, lb/hr:	0.5	0.5	0.5	0.38	0.36	0.34
SO2, ppmv:	0.44	0.47	0.47	0.3	0.3	0.3
TSP, lb/hr:	1.5	1.5	1.3	2.8	2.7	2.5
PM-10, lb/hr:	1.5	1.5	1.3	AP-42	2.8	2.8

STACK PARAMETERS

Load:		100%	
Ambient Temperature, F.	0	50	100
Conditioning:	0	50	100
Velocity, m/sec	25.5	25.92	23.78
Stack Temp, K	737.44	787.44	805.22
NOx, g/sec	2.900	2.930	2.530
CO, g/sec	7.000	3.780	1.240
PM, g/sec	0.190	0.190	0.170
SO2, g/sec	0.070	0.070	0.060

Annual Emissions

Load:		100%	
Ambient Temperature, F.	0	50	100
Conditioning:	0	50	100
Annual hours (Each Turbine)			
Updated Analysis Based on Total Permitted Fuel (All 3 Turbines Combined)			
Natural Gas			
Max Fuel Firing Rate (scf/hr)	251,000		
Max Fuel Consumption (scf)	540,905,000		
Liquid Fuel			
Max Fuel Firing Rate (gal/hr)	1,800		
Max Fuel Consumption (gal)	2,249,100		
Annual Hours (Each Turbine)	718	718	718
Emissions are totals for three units			
NOx (tpy)	24.78	25.00	21.66
CO (tpy)	59.80	32.33	10.56
VOC (tpy)	3.12	3.12	2.69
PM (tpy)	1.63	1.64	1.42
SC2 (tpy)	0.58	0.58	0.50

PERMIT LIMITS

Maximum Gross Heat Input (mmBtu/hr)	246.6
NOx (lb/mmBtu)	0.091
CO (lb/mmBtu)	0.117
VOC (lb/mmBtu)	0.011
PM (lb/mmBtu)	0.006
SC2 (lb/mmBtu)	0.002

HAPs

Natural Gas 100%		Oil 100%	
Fuel	Lead:		
Ambient Temperature, F:			
Engine Net Temperature:			
Conditioning:			

Natural Gas 100%		Oil 100%	
Fuel	Lead:		
0	0	90	90
0	NONE	90	90
NONE	NONE	NONE	NONE

HAP's (lb/MMBtu)

Source

Formaldehyde	1	9.13E-05	9.13E-05	9.13E-05	9.13E-05	9.13E-05	9.13E-05
1,3 Butadiene	2	4.30E-07	4.30E-07	4.30E-07	1.60E-05	1.60E-05	1.60E-05
Acetaldehyde	2	4.00E-05	4.00E-05	4.00E-05	NA	NA	NA
Benzene	2	1.20E-05	1.20E-05	1.20E-05	5.50E-05	5.50E-05	5.50E-05
Ethylbenzene	2	3.20E-05	3.20E-05	3.20E-05	NA	NA	NA
Naphthalene	2	1.30E-06	1.30E-06	1.30E-06	3.50E-05	3.50E-05	3.50E-05
PAH (Total)	2	2.20E-06	2.20E-06	2.20E-06	4.00E-05	4.00E-05	4.00E-05
PAH (BS)	4	4.84E-08	4.84E-08	4.84E-08	5.20E-07	5.20E-07	5.20E-07
CPV	4	8.58E-08	8.58E-08	8.58E-08	5.20E-07	5.20E-07	5.20E-07
Propylene Oxide	2	2.90E-05	2.90E-05	2.90E-05	NA	NA	NA
Toluene	2	1.30E-04	1.30E-04	1.30E-04	NA	NA	NA
Xylenes	2	6.40E-05	6.40E-05	6.40E-05	NA	NA	NA
Arsenic	3	NA	NA	NA	4.00E-07	4.00E-07	4.00E-07
Beryllium	3	NA	NA	NA	8.00E-08	8.00E-08	8.00E-08
Cadmium	3	NA	NA	NA	3.20E-06	3.20E-06	3.20E-06
Chromium	2	NA	NA	NA	1.10E-05	1.10E-05	1.10E-05
Lead	3	NA	NA	NA	1.40E-05	1.40E-05	1.40E-05
Manganese	3	NA	NA	NA	1.60E-04	1.60E-04	1.60E-04
Mercury	2	NA	NA	NA	1.20E-06	1.20E-06	1.20E-06
Nickel	2	NA	NA	NA	4.60E-06	4.60E-06	4.60E-06
Selenium	2	NA	NA	NA	2.50E-05	2.50E-05	2.50E-05
Sulfuric Acid	5	1.72E-04	1.72E-04	1.72E-04	2.72E-05	2.72E-05	2.72E-05

Natural Gas 100%		Oil 100%	
Fuel	Lead:		
9.13E-05	9.13E-05	9.13E-05	9.13E-05
4.30E-07	4.30E-07	4.30E-07	1.60E-05
4.00E-05	4.00E-05	4.00E-05	NA
1.20E-05	1.20E-05	1.20E-05	5.50E-05
3.20E-05	3.20E-05	3.20E-05	NA
1.30E-06	1.30E-06	1.30E-06	3.50E-05
2.20E-06	2.20E-06	2.20E-06	4.00E-05
4.84E-08	4.84E-08	4.84E-08	5.20E-07
8.58E-08	8.58E-08	8.58E-08	5.20E-07
2.90E-05	2.90E-05	2.90E-05	NA
1.30E-04	1.30E-04	1.30E-04	NA
6.40E-05	6.40E-05	6.40E-05	NA
NA	NA	NA	4.00E-07
NA	NA	NA	4.00E-07
NA	NA	NA	8.00E-08
NA	NA	NA	3.20E-06
NA	NA	NA	1.10E-05
NA	NA	NA	1.40E-05
NA	NA	NA	1.60E-04
NA	NA	NA	1.20E-06
NA	NA	NA	4.60E-06
NA	NA	NA	2.50E-05
1.72E-04	1.72E-04	1.72E-04	2.72E-05

Fuel Load:
Ambient Temperature, F:
Engine Inlet Temperature:
Conditioning:

Natural Gas 100%		
0	50	100
0	50	100
NONE	NONE	NONE

Oil 100%		
90	90	90
90	90	90
NONE	NONE	NONE

WAP's (lb/hr)(per turbine)

Formaldehyde									
1,3 Butadiene									
Acetaldehyde									
Benzene									
Ethylbenzene									
Naphthalene									
PAH (Total)									
PAH (BS)									
C _{TPV}									
Propylene Oxide									
Toluene									
Xylenes									
Arsenic									
Beryllium									
Cadmium									
Chromium									
Lead									
Manganese									
Mercury									
Nickel									
Selenium									
Sulfuric Acid									

Oil 100%									
0	50	100	100	100	100	100	100	100	100
NONE	NONE	NONE	NONE	NONE	NONE	NONE	NONE	NONE	NONE

Fuel Load:
Ambient Temperature, F:
Engine inlet temperature:
Conditioning

HAP's (g/s)(per turbine)

Formaldehyde								
1,3 Butadiene								
Acetaldehyde								
Benzene								
Ethylbenzene								
Naphthalene								
PAH (Total)								
PAH (BS)								
CTPV								
Propylene Oxide								
Toluene								
Xylenes								
Arsenic								
Beryllium								
Cadmium								
Chromium								
Lead								
Manganese								
Mercury								
Nickel								
Selenium								
Sulfuric Acid								

	Natural Gas 100%							
0	0	50	100	100	90	90	90	90
0	0	50	100	100	NONE	NONE	NONE	NONE
NONE	NONE	NONE	NONE	NONE	NONE	NONE	NONE	NONE

0	0	50	100	100	90	90	90	90
0	0	50	100	100	NONE	NONE	NONE	NONE
NONE								

0	0	50	100	100	90	90	90	90
0	0	50	100	100	NONE	NONE	NONE	NONE
NONE								

2.64E-03	2.66E-03	2.30E-03	2.68E-03	2.55E-03	2.43E-03	2.66E-03	2.66E-03	2.25E-03
1.24E-05	1.23E-05	1.08E-05	4.71E-04	4.47E-04	4.26E-04	4.66E-04	4.66E-04	3.95E-04
1.16E-03	1.17E-03	1.01E-03	-0.009E+00	0.009E+00	0.009E+00	0.009E+00	0.009E+00	0.009E+00
3.47E-04	3.50E-04	3.02E-04	1.62E-03	1.53E-03	1.46E-03	1.60E-03	1.60E-03	1.36E-03
9.26E-04	9.33E-04	8.05E-04	0.009E+00	0.009E+00	0.009E+00	0.009E+00	0.009E+00	0.009E+00
3.76E-05	3.79E-05	3.27E-05	1.03E-03	9.77E-04	9.31E-04	1.02E-03	1.02E-03	8.63E-04
6.36E-05	6.41E-05	5.53E-05	1.18E-03	1.12E-03	1.06E-03	1.17E-03	1.16E-03	9.86E-04
1.40E-06	1.41E-06	1.22E-06	1.53E-05	1.45E-05	1.38E-05	1.52E-05	1.51E-05	1.28E-05
2.48E-06	2.50E-06	2.16E-06	1.53E-05	1.45E-05	1.38E-05	1.52E-05	1.51E-05	1.28E-05
8.39E-04	8.45E-04	7.29E-04	NA	NA	NA	NA	NA	NA
3.76E-03	3.79E-03	3.27E-03	NA	NA	NA	NA	NA	NA
1.85E-03	1.87E-03	1.61E-03	NA	NA	NA	NA	NA	NA
NA	NA	NA	1.18E-05	1.12E-05	1.06E-05	1.17E-05	1.16E-05	9.86E-06
NA	NA	NA	2.35E-06	2.23E-06	2.13E-06	2.33E-06	2.33E-06	1.97E-06
NA	NA	NA	9.41E-05	8.93E-05	8.51E-05	9.33E-05	9.32E-05	7.89E-05
NA	NA	NA	3.23E-04	3.07E-04	2.99E-04	3.21E-04	3.20E-04	2.71E-04
NA	NA	NA	4.12E-04	3.91E-04	3.72E-04	4.08E-04	4.08E-04	3.45E-04
NA	NA	NA	4.71E-03	4.47E-03	4.26E-03	4.66E-03	4.66E-03	3.95E-03
NA	NA	NA	3.53E-05	3.35E-05	3.19E-05	3.50E-05	3.49E-05	2.96E-05
NA	NA	NA	1.35E-04	1.28E-04	1.22E-04	1.34E-04	1.34E-04	1.13E-04
NA	NA	NA	7.35E-04	6.98E-04	6.65E-04	7.29E-04	7.28E-04	6.16E-04
4.96E-03	5.00E-03	4.31E-03	8.01E-04	7.66E-04	7.24E-04	7.93E-04	7.93E-04	6.71E-04

Fuel Load:
Ambient Temperature, F:
Engine inlet Temperature:
Conditioning:

Natural Gas 100%		
0	50	100
0	50	100
NONE	NONE	NONE

Oil 100%		
90	90	90
90	90	90
NONE	NONE	NONE

UPDATED TO REFLECT MODIFIED OPERATION HOURS

HAP's (tpy)(per turbine)

Formaldehyde	7.53E-03	7.38E-03	6.55E-03	4.44E-03	4.21E-03	4.01E-03	4.40E-03	4.39E-03	3.72E-03
1,3 Butadiene	3.55E-05	3.57E-05	3.08E-05	7.78E-04	7.38E-04	7.03E-04	7.71E-04	7.70E-04	6.52E-04
Acetaldehyde				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Benzene	3.30E-03	3.32E-03	2.87E-03	2.67E-03	2.54E-03	2.42E-03	2.65E-03	2.65E-03	2.24E-03
Ethylbenzene	9.90E-04	9.97E-04	8.60E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Naphthalene	2.64E-03	2.66E-03	2.29E-03	1.70E-03	1.61E-03	1.54E-03	1.69E-03	1.68E-03	1.43E-03
PAH (Total)	1.07E-04	1.08E-04	9.32E-05	1.81E-04	1.83E-04	1.58E-04	1.94E-03	1.85E-03	1.76E-03
PAH (BS)	3.99E-06	4.02E-06	3.47E-06	5.28E-03	5.23E-05	2.40E-05	2.53E-05	2.40E-05	2.29E-05
CTPV	7.08E-06	7.13E-06	6.15E-06	2.39E-03	2.41E-03	2.08E-03	2.53E-05	2.40E-05	2.29E-05
Propylene Oxide				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Toluene	1.07E-02	1.08E-02	9.32E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Xylenes	5.28E-03	5.32E-03	4.59E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Arsenic	0.00E+00	0.00E+00	0.00E+00	1.94E-05	1.83E-05	1.76E-05	1.93E-05	1.93E-05	1.63E-05
Beryllium	0.00E+00	0.00E+00	0.00E+00	3.89E-06	3.59E-06	3.52E-06	3.85E-06	3.85E-06	3.26E-06
Cadmium	0.00E+00	0.00E+00	0.00E+00	1.56E-04	1.48E-04	1.41E-04	1.54E-04	1.54E-04	1.30E-04
Chromium	0.00E+00	0.00E+00	0.00E+00	5.35E-04	5.07E-04	4.84E-04	5.30E-04	5.29E-04	4.48E-04
Lead	0.00E+00	0.00E+00	0.00E+00	6.80E-04	6.46E-04	6.15E-04	6.74E-04	6.74E-04	5.71E-04
Manganese	0.00E+00	0.00E+00	0.00E+00	7.78E-03	7.38E-03	7.03E-03	7.71E-03	7.70E-03	6.52E-03
Mercury	0.00E+00	0.00E+00	0.00E+00	5.83E-05	5.54E-05	5.28E-05	5.78E-05	5.78E-05	4.89E-05
Nickel	0.00E+00	0.00E+00	0.00E+00	2.24E-04	2.12E-04	2.02E-04	2.22E-04	2.21E-04	1.87E-04
Selenium	0.00E+00	0.00E+00	0.00E+00	1.22E-03	1.15E-03	1.10E-03	1.20E-03	1.20E-03	1.02E-03
Sulfuric Acid	1.41E-02	1.43E-02	1.23E-02	1.32E-03	1.26E-03	1.20E-03	1.31E-03	1.31E-03	1.11E-03
Total HAPS	0.047329179	0.047679613	0.04114505	0.0235757	0.0225737	0.021323	0.0233636	0.0233434	0.0197677

Source Notes:

- Background document for AP-42 Section 3.1
- AP-42 Sections 3.1
- Fuel Analysis
- Calculated using CT DEP memo regarding Interim PAH Policy
- Calculated using CT DEP Nash Memo

ATTACHMENT E-5. CALCULATION OF % PAH BENZENE SOLUBLE AND
CTPV FOR SPECIATED COMPOUNDS FROM NATURAL GAS COMBUSTION¹

CAS No.	Compound	PAH?	Benzene Soluble PAH? ²	CTPV? ²	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
91-57-6	2-Methylnaphthalene ^{3,4}	Yes	No	No	2.4E-05	D
56-49-5	3-Methylchloranthrene ^{3,4}	Yes	No	No	1.8E-06	E
	7,12-Dimethylbenz(a)anthracene ^{3,4}	Yes	No	No	1.6E-05	E
83-32-9	Acenaphthene ^{3,4}	Yes	No	No	1.8E-06	E
203-96-8	Acenaphthylene ^{3,4}	Yes	No	No	1.8E-06	E
120-12-7	Anthracene ^{3,4}	Yes	No	Yes	2.4E-06	E
56-55-3	Benz(a)anthracene ^{3,4}	Yes	Yes	No	1.8E-06	E
71-43-2	Benzene ³	No	No	No	2.1E-03	B
50-32-8	Benzo(a)pyrene ^{3,4}	Yes	Yes	Yes	1.2E-06	E
205-99-2	Benzo(b)fluoranthene ^{3,4}	Yes	Yes	No	1.8E-06	E
191-24-2	Benzo(g,h,i)perylene ^{3,4}	Yes	Yes	No	1.2E-06	E
205-82-3	Benzo(k)fluoranthene ^{3,4}	Yes	Yes	No	1.8E-06	E
106-97-8	Butane	No	No	No	2.1	E
218-01-9	Chrysene ^{3,4}	Yes	Yes	Yes	1.8E-06	E
53-70-3	Dibenzo(a,h)anthracene ^{3,4}	Yes	Yes	No	1.2E-06	E
25321-22-6	Dichlorobenzene ³	No	No	No	1.2E-03	E
74-84-0	Ethane	No	No	No	3.1	E
206-44-0	Fluoranthene ^{3,4}	Yes	Yes	No	3.0E-06	E
86-73-7	Fluorene ^{3,4}	Yes	No	No	2.8E-06	E
50-00-0	Formaldehyde ³	No	No	No	7.5E-02	B
110-54-3	Hexane ³	No	No	No	1.8	E
193-39-5	Ideno(1,2,3-cd)pyrene ^{3,4}	Yes	Yes	No	1.8E-06	E
91-20-3	Naphthalene ³	Yes	No	No	6.1E-04	E
109-66-0	Pentane	No	No	No	2.6	E
85-01-8	Phenanathrene ^{3,4}	Yes	No	Yes	1.7E-05	D
74-98-6	Propane	No	No	No	1.6	E
129-00-0	Pyrene ^{3,4}	Yes	No	Yes	5.0E-06	E
108-88-3	Toluene ³	No	No	No	3.4E-03	C

TOTAL PAH = 6.98E-04 lb/10⁶ scf

BENZENE SOLUBLE PAH = 1.56E-05 lb/10⁶ scf (2.2% of PAH)

CTPV PAH = 2.74E-05 lb/10⁶ scf (3.9% of PAH)

¹ From AP-42 (July, 1998), Table 1.4-3

² "Interim PAH Policy," DEP Memo from John Gove to Leonard Bruckman dated March 30, 1990

³ Hazardous Air Pollutant (HAP) as defined by Section 112(b) of the Clean Air Act

⁴ HAP because it is polycyclic organic matter (POM). POM is a HAP as defined by Section 112(b) of the Clean Air Act

ATTACHMENT E-6 CALCULATION OF % PAH BENZENE SOLUBLE AND CTPV
FOR SPECIATED COMPOUNDS FROM LIQUID FUEL COMBUSTION¹

CAS No.	Compound	PAH?	Benzene Soluble PAH? ²	CTPV? ²	Emission Factor (lb/10 ³ gal)	Emission Factor Rating
71-43-2	Benzene	No	No	No	2.14E-04	C
100-41-4	Ethylbenzene	No	No	No	6.36E-05	E
50-00-0	Formaldehyde ³	No	No	No	3.30E-02	C
91-20-3	Naphthalene ³	Yes	No	No	1.13E-03	C
71-55-6	1,1,1-Trichloroethane	Yes	No	No	2.36E-04	E
108-88-3	Toluene	No	No	No	6.20E-03	D
95-47-6	0-Xylene	No	No	No	1.09E-04	E
83-32-9	Acenaphthene	Yes	No	No	2.11E-05	C
203-96-8	Acenaphthylene	Yes	No	No	2.53E-07	D
120-12-7	Anthracene	Yes	No	Yes	1.22E-06	C
56-55-3	Benz(a)anthracene	Yes	Yes	No	4.01E-06	C
205-99-2	Benzo(b,k)fluoranthene	Yes	Yes	No	1.48E-06	C
191-24-2	Benzo(g,h,i)perylene	Yes	Yes	No	2.26E-06	C
218-01-9	Chrysene	Yes	Yes	Yes	2.38E-06	C
53-70-3	Dibenzo(a,h)anthracene	Yes	Yes	No	1.67E-06	D
206-44-0	Fluoranthene	Yes	Yes	No	4.84E-06	C
86-73-7	Fluorene	Yes	No	No	4.47E-06	C
193-39-5	Indeno(1,2,3-cd)pyrene	Yes	Yes	No	2.14E-06	C
85-01-8	Phenanthrene	Yes	No	Yes	1.05E-05	C
129-00-0	Pyrene	Yes	No	Yes	4.25E-06	C
109-66-0	OCDD	No	No	No	3.10E-09	E

TOTAL PAH = 1.43E-03 lb/10³ gal

BENZENE SOLUBLE PAH = 1.88E-05 lb/10³ gal (1.3% of PAH)

CTPV PAH = 1.84E-05 lb/10³ gal (1.3% of PAH)

¹ From AP-42 (September, 1998), Table 1.3-9

² "Interim PAH Policy," DEP Memo from John Gove to Leonard Bruckman dated March 30, 1990

Intertek Testing Services
Caleb Brett

Report of Analysis

Submission: 2003-001096-NYHB
 Customer: Connecticut Municipal Elec. Energy Cooperative
 Terminal: SUN NEWARK, NJ
 Vessel: SHORE TANK # 24
 Purchase Order: 6480
 Date Received: March 28, 2003
 Date Reported: April 14, 2003

Method	Test	Results	Units
D4052	API Gravity @ 60 Deg F	42.6	deg API
D93 method A	Corrected Flash Point	131	deg F
D4294	Sulfur	0.00250	Wt %
D240	Gross Heat of Combustion	19,314	BTU/lb
D240	Gross Heat of Combustion	134,081	BTU/gal
D482 (2) 775 deg C	Ash (@ 775 deg C)	<0.001	Wt %
D4377	Water Content	3.58	ppm
D3803	Lead	<0.1	ppm (mg/L)
D3605	Sodium	<0.1	ppm (mg/L)
D3605	Vanadium	<0.1	ppm (mg/L)
D130	Copper Corrosion @ 50 °C for 3 hrs	1a	
D1796	Sediment and Water	0.05	Vol %
D5762	Nitrogen	<10	ppm
D5452/2276	Particulate Matter	3.90	mg/l
D1018 Mod	Hydrogen	13.75	Wt %
GFAA	Beryllium	<0.2	ppb (µg/kg)
GFAA	Cadmium	<0.36	ppb (µg/kg)
D5208	Potassium	<0.3	ppm (mg/kg)
H885	Manganese	<0.1	ppm (mg/kg)
H885	Aluminum	<10	ppb (mg/L)
D1401	Temperature	-54	deg C
D1401	Sample	40	mls
D1401	Water	40	mls
D1401	Exudate	0	mls
D1401	Time	5	min
D324	Combustion Residue on 10% Dist. Res.	0.06	Wt %


 4/14/03
 HWA/CB
 Howard W. Apel II, Laboratory Manager

April 14, 2003

ATTACHMENT E-8. MASC STACK CONCENTRATION CALCULATIONS - UNIT #1 - GASEOUS FUEL

Waterside Power, LLC
Unit #1 - Gaseous Fuel
100% Load, 50F ambient

Stack Height	X	<20 meters 131 feet (distance to property line)	MASC = 0.885*HLV*(X + 1.08*(V**0.64))**1.56/V
Airflow	V	345,274 ACFM per unit 9777 m^3/min 162.95 m^3/s 586627 m^3/hr 4.54E+08 ug	
	1 lb =		
	dilution factor:	4 (MASC/HLV)	

Calculate allowable metals concentration from MASC allowable emissions.
255.60 MMBtu/hr/unit, HHV (approx)

	8-HR HLV (ground level) ug/m^3	MASC (stack) ug/m^3	Emission Factor lb/MMBtu	Predicted emissions (stack) lb/hr	Predicted emissions (stack) ug/m^3
Formaldehyde	12	47	9.10E-05	2.33E-02	17.99 good
1,3 Butadiene	22000	86,415	4.30E-07	1.10E-04	0.08 good
Acetdehyde	3600	14,141	4.00E-05	1.02E-02	7.91 good
Benzene	150	589	1.20E-05	3.07E-03	2.37 good
Ethylbenzene	8700	34,173	3.20E-05	8.18E-03	6.32 good
Naphthalene	1000	3,928	1.30E-06	3.32E-04	0.26 good
PAH (Benzene Soluble)	0.1	0.4	4.84E-08	1.24E-05	0.01 good
Coal Tar Pitch Volatiles	1	4	8.60E-08	2.20E-05	0.02 good
Propylene Oxide	1000	3,928	2.90E-05	7.41E-03	5.73 good
Toluene	7500	29,460	1.30E-04	3.32E-02	25.69 good
Xylenes	8680	34,095	6.40E-05	1.64E-02	12.65 good
Sulfuric Acid	20	79	1.72E-04	4.40E-02	33.99 good

Note: Sulfuric Acid based on 11/27/87 CT DEP Nash memo and assuming 0.8 grains of S per 100 cu. Ft., 5% conversion rate of S to SO₃, and 1020 Btu per cu. Ft.: H₂SO₄ emission factor = 0.8 gr S/100 cu. Ft. X 1 cu. ft/1020 Btu X 1 lb/7000 gr. S X 1x10⁶ Btu/MMBtu X 0.05 lbs S/1 lb Mol H₂SO₄/32 lb-mol S = 4.2892 E-05 lb

HLV values from Tables 29-1, 29-2, or 29-3 of RCSCA Section 22a-174-29.
Trace organic emission factors from AP-42, Section 3.1

ATTACHMENT E-9. MASC STACK CONCENTRATION CALCULATIONS - UNIT #2 - GASEOUS FUEL

Waterside Power, LLC
Unit #2 - Gaseous Fuel
100% Load, 50F ambient

Stack Height X	<20 meters 117 feet (distance to property line) 35.7 meters (distance to property line)	MASC = 0.885*HLV*(X + 1.08*(V**0.64))**1.56/V
Airflow V	345,274 ACFM per unit 9777 m^3/min 162.95 m^3/s 586627 m^3/hr 4.54E+08 ug	
	1 lb = dilution factor: 4 (MASC/HLV)	

Calculate allowable metals concentration from MASC allowable emissions.
255.60 MMBtu/hr/unit, HHV (approx)

	8-HR HLV (ground level) ug/m^3	MASC (stack) ug/m^3	Emission Factor lb/MMBtu	Predicted emissions (stack) lb/hr	Predicted Conc. (stack) ug/m^3
Formaldehyde	12	43	9.10E-05	2.33E-02	17.99 good
1,3 Butadiene	22000	78,112	4.30E-07	1.10E-04	0.08 good
Acetadehyde	3600	12,782	4.00E-05	1.02E-02	7.91 good
Benzene	150	533	1.20E-05	3.07E-03	2.37 good
Ethylbenzene	8700	30,890	3.20E-05	8.18E-03	6.32 good
Naphthalene	1000	3,551	1.30E-06	3.32E-04	0.26 good
PAH (Benzene Soluble)	0.1	0.4	4.84E-08	1.24E-05	0.01 good
Coal Tar Pitch Volatiles	1	4	8.60E-08	2.20E-05	0.02 good
Propylene Oxide	1000	3,551	2.90E-05	7.41E-03	5.73 good
Toluene	7500	26,629	1.30E-04	3.32E-02	25.69 good
Xylenes	8680	30,819	6.40E-05	1.64E-02	12.65 good
Sulfuric Acid	20	71	1.72E-04	4.40E-02	33.99 good

Note: Sulfuric Acid based on 11/27/87 CT DEP Nash memo and assuming 0.8 grains of S per 100 cu. ft., 5% conversion rate of S to SO₃, and 1020 Btu per cu. ft.; H₂SO₄ emission factor = 0.8 gr S/100 cu. ft. X 1 cu. ft/1020 Btu X 1 lb/7000 gr. S X 1x10⁻⁶ Btu/MMBtu X 0.05 lbs S/1 lb S X 98 lb-Mol H₂SO₄/32 lb-mol S = 4.2892 E-05 lb

HLV values from Tables 29-1, 29-2, or 29-3 of RCSA Section 22a-174-29.
Trace organic emission factors from AP-42, Section 3.1

ATTACHMENT E-10. MASC STACK CONCENTRATION CALCULATIONS - UNIT #3 - GASEOUS FUEL

Waterside Power, LLC
Unit #3 - Gaseous Fuel
100% Load, 50F ambient

Stack Height	X	<20 meters 113 feet (distance to property line)	MASC = 0.885*H _{LV} * $(X + 1.08*(V^{**}0.64))^{**}1.56/V$
Airflow	V	34.4 meters (distance to property line) 345,274 ACFM per unit 9777 m ³ /min 162.95 m ³ /s 58627 m ³ /hr 4.54E+08 ug	
		1 lb =	3 (MASC/H _{LV})
		dilution factor:	

Calculate allowable metals concentration from MASC allowable emissions.
255.60 MM Btu/hr/unit, HHV (approx)

	8-HR H _{LV} (ground level)	MASC (stack) ug/m ³	AP-42 Emission Factor lb/MMBtu	Predicted emissions (stack) lb/hr	Predicted Conc. (stack) ug/m ³
Formaldehyde	12	41	9.10E-05	2.33E-02	17.99 good
1,3 Butadiene	22000	75,796	4.30E-07	1.10E-04	0.08 good
Acetaldehyde	3600	12,403	4.00E-05	1.02E-02	7.91 good
Benzene	150	517	1.20E-05	3.07E-03	2.37 good
Ethylbenzene	8700	29,974	3.20E-05	8.18E-03	6.32 good
Naphthalene	1000	3,445	1.30E-06	3.32E-04	0.26 good
PAH (Benzene Soluble)	0.1	0.3	4.84E-08	1.24E-05	0.01 good
Coal Tar Pitch Volatiles	1	3	8.60E-08	2.20E-05	0.02 good
Propylene Oxide	1000	3,445	2.90E-05	7.41E-03	5.73 good
Toluene	7500	25,839	1.30E-04	3.32E-02	25.69 good
Xylenes	8680	29,905	6.40E-05	1.64E-02	12.65 good
Sulfuric Acid	20	69	1.72E-04	4.40E-02	33.99 good

Note: Sulfuric Acid based on 11/27/87 CT DEP Nash memo and assuming 0.8 grains of S per 100 cu. ft., 5% conversion rate of S to SO₃, and 1020 Btu per cu. ft.: H₂SC₄ emission factor = 0.8 gr S/100 cu. ft. X 1 cu. ft/1020 Btu X 1 lb/7000 gr. S X 1x10⁶ Btu/MMBtu X 0.05 lbs S/1 lb S X 98 lb-Mol H₂SO₄/32 lb-mol S = 4.2892 E-05 lb

HLV values from Tables 29-1, 29-2, or 29-3 of RCSA Section 22a-174-29.
Trace organic emission factors from AP-42, Section 3.1

ATTACHMENT E-11. MASC STACK CONCENTRATION CALCULATIONS - UNIT #1 - LIQUID FUEL

Waterside Power, LLC
Unit #1 - Liquid Fuel
100% Load, 50F Ambient

Stack Height X	<20 meters 131 feet (distance to property line) 39.9 meters (distance to property line)	MASC = $0.885^*HVL^*(X + 1.08^*(V^*0.64))^**1.56/V$
Airflow V	341,683 ACFM per unit 9675 m ³ /min 161.26 m ³ /s 580526 m ³ /hr 4.54E+08 ug dilution factor: 4 (MASC/HLV)	Sulfuric Acid Emissions: 246.58 MMBtu/hr, HHV (approx.) 135,000 Btu/gal liquid fuel, typical 1844.0 gal/hr liquid fuel flow
1 lb = 246.58 MMBtu/hr/unit, HHV (approx) 18,500 Btu/lb liquid fuel, typical 13,329 lb/hr liquid fuel flow, estimated		0.0015 % S in oil 0.003675 lb H ₂ SO ₄ emitted/thousand gallons fuel fired (based on 11/27/87 memo H ₂ SO ₄ = 27(S)*1,225 lb/1000 gal) 0.0068 lb/hr H ₂ SO ₄ emitted based on 11/27/87 memo

Calculate allowable metals concentration from MASC allowable emissions.
246.58 MMBtu/hr/unit, HHV (approx)
18,500 Btu/lb liquid fuel, typical
13,329 lb/hr liquid fuel flow, estimated

Trace Organic Emission Factors from AP-42 Table 3-3-2, 10/96

	8-HR HLV (ground level) ug/m ³	MASC (stack) ug/m ³	AP-42 Emission Factor lb/MMBtu	Predicted emissions (stack) lb/hr	Predicted Conc. (stack) ug/m ³
Formaldehyde	12	47	9.10E-05	2.24E-02	17.53 good
1,3 Butadiene	22000	86,948	1.60E-05	3.95E-03	3.08 good
Benzene	150	593	5.50E-05	1.36E-02	10.60 good
Naphthalene	1000	3,952	3.50E-05	8.63E-03	6.74 good
PAH (Benzene Soluble)	0.1	0.4	5.20E-07	1.28E-04	0.10 good
Coal Tar Pitch Volatiles	1	4	5.20E-07	1.28E-04	0.10 good
Arsenic	0.05	0.2	4.00E-07	9.86E-05	0.08 good
Beryllium	0.01	0.04	8.00E-08	1.97E-05	0.02 good
Cadmium	0.4	2	3.20E-06	7.89E-04	0.62 good
Chromium	2.5	10	1.10E-05	2.71E-03	2.12 good
Lead	3	12	1.40E-05	3.45E-03	2.70 good
Manganese	20	79	1.60E-04	3.95E-02	30.83 good
Mercury	1	4	1.20E-06	2.96E-04	0.23 good
Nickel	5	20	4.60E-06	1.13E-03	0.89 good
Selenium	4	16	2.50E-05	6.16E-03	4.82 good
Sulfuric Acid	20	79	—	6.78E-03	5.30 good

Notes:

See Attachment E-7 For ultra-low sulfur fuel grab sample results (Source: South Norwalk Electric Works NSR Permit Application dated April 2003)
Sulfuric Acid Emission Factor from 11/27/97 CTDEP memo
HLV values from Tables 29-1, 29-2, or 29-3 of RCSA Section 22a-174-29.
Trace organic emission factors from AP-42, Section 3.1

ATTACHMENT E-12. MASC STACK CONCENTRATION CALCULATIONS - UNIT #2 - LIQUID FUEL

Waterside Power, LLC
Unit #2 - Liquid Fuel
100% Load, 50F Ambient

Stack Height X	<20 meters 117 feet (distance to property line) 35.7 meters (distance to property line)	MASC = $0.885^*H\bar{L}V^*(X + 1.08^*(V^*0.64))^**1.56/V$
Airflow V	341,683 ACFM per unit 9675 m ³ /min 161.26 m ³ /s 580526 m ³ /hr 4.54E+08 ug	Sulfuric Acid Emissions: 246.58 MMBtu/hr, HHV (approx.) 135,000 Btu/gal liquid fuel, typical 1844.0 gal/hr liquid fuel flow
1 lb = dilution factor:	4 (MASC/HLV)	0.0015 % S in oil 0.003675 lb H ₂ SO ₄ emitted/thousand gallons fuel fired (based on 11/27/87 memo H ₂ SO ₄ = 27(S)*1.225 lb/1000 gal) 0.0068 lb/hr H ₂ SO ₄ emitted based on 11/27/87 memo
Calculate allowable metals concentration from MASC allowable emissions. 246.58 MMBtu/hr/unit, HHV (approx) 18,500 Btu/lb liquid fuel, typical 13,329 lb/hr liquid fuel flow, estimated		

Trace organic emission factors from AP-42 Table 3-3-2, 10/96
8-HR HLV
(ground level)
ug/m³

Formaldehyde	AP-42	Predicted emissions (stack)	
1,3 Butadiene	Emission Factor lb/MMBtu	lb/hr	
Benzene	ug/m ³	ug/m ³	
Naphthalene	12	43	17.53 good
PAH (Benzene Soluble)	22000	78,571	3.95E-03 3.08 good
Coal Tar Pitch Volatiles	150	536	5.50E-05 2.24E-02 10.60 good
Arsenic	1000	3,571	3.50E-05 1.36E-02 6.74 good
Beryllium	0.1	0.4	8.63E-03 1.28E-04 0.10 good
Cadmium	1	4	5.20E-07 1.28E-04 0.10 good
Chromium	0.05	0.2	4.00E-07 9.86E-05 0.08 good
Lead	0.01	0.04	8.00E-08 1.97E-05 0.02 good
Manganese	3	11	1.10E-05 2.71E-03 2.12 good
Mercury	20	71	1.40E-05 3.45E-03 2.70 good
Nickel	1	4	1.60E-04 3.95E-02 30.83 good
Selenium	5	18	4.60E-06 7.89E-04 0.62 good
Sulfuric Acid	4	14	2.50E-05 6.16E-03 4.82 good
	20	71	— 6.78E-03 5.30 good

Notes:

See Attachment E-7 For ultra-low sulfur fuel grab sample results (Source: South Norwalk Electric Works NSR Permit Application dated April 2003)
Sulfuric Acid Emission Factor from 11/27/97 CTDEP memo
HLV values from Tables 29-1, 29-2, or 29-3 of RCSA Section 22a-174-29.
Trace organic emission factors from AP-42, Section 3.1

ATTACHMENT E-13. MASC STACK CONCENTRATION CALCULATIONS - UNIT #3 - LIQUID FUEL

Waterside Power, LLC
Unit #3 - Liquid Fuel
100% Load, 50F Ambient

Stack Height X	<20 meters	MASC = $0.885^*HLV^*(X + 1.08^*(M^*0.64))^**1.56/V$
	113 feet (distance to property line)	
	34.4 meters (distance to property line)	
Airflow	341,683 ACFM per unit	
V	9675 m^3/min	Sulfuric Acid Emissions:
	161.26 m^3/s	246.58 MMBl/hr, HHV (approx.)
	580526 m^3/hr	135,000 Btu/gal liquid fuel, typical
1 lb =	4.54E+08 ug	1844.0 gal/hr liquid fuel flow
dilution factor:	3 (MASC/HLV)	

Calculate allowable metals concentration from MASC allowable emissions.
246.58 MMBl/hr/unit, HHV (approx)
18,500 Btu/lb liquid fuel, typical
13,329 lb/hr liquid fuel flow, estimated

Stack Height X	<20 meters	MASC = $0.885^*HLV^*(X + 1.08^*(M^*0.64))^**1.56/V$
	113 feet (distance to property line)	
	34.4 meters (distance to property line)	
Airflow	341,683 ACFM per unit	
V	9675 m^3/min	Sulfuric Acid Emissions:
	161.26 m^3/s	246.58 MMBl/hr, HHV (approx.)
	580526 m^3/hr	135,000 Btu/gal liquid fuel, typical
1 lb =	4.54E+08 ug	1844.0 gal/hr liquid fuel flow
dilution factor:	3 (MASC/HLV)	

0.0015 % S in oil
0.003675 lb H₂SO₄ emitted/thousand gallons fuel fired
(based on 11/27/87 memo H₂SO₄ = 2*(S)*1.225 lb/1000 gal)
0.0068 lb/hr H₂SO₄ emitted based on 11/27/87 memo

	AP-42 Emission Factor (stack)	Predicted emissions (stack)	Predicted Conc. (stack)
	ug/m^3	lb/MMBtu	ug/m^3
Formaldehyde	12	9.10E-05	2.24E-02
1,3 Butadiene	42	1.60E-05	3.95E-03
Benzene	22000	76.234	17.53 good
Naphthalene	150	5.50E-05	3.08 good
PAH (Benzene Soluble)	1000	3.465	1.36E-02
Coal Tar Pitch Volatiles	0.1	0.3	8.63E-03
Arsenic	1	5.20E-07	6.74 good
Beryllium	0.05	0.2	1.28E-04
Cadmium	0.01	0.03	0.10 good
Chromium	0.4	1	3.20E-06
Lead	2.5	9	1.10E-05
Manganese	3	10	2.71E-03
Mercury	20	69	2.12 good
Nickel	1	3	7.89E-04
Selenium	5	17	0.62 good
Sulfuric Acid	4	14	6.16E-03
	20	69	4.82 good
		—	6.78E-03
			5.30 good

Notes:

See Attachment E-7 For ultra-low sulfur fuel grab sample results (Source: South Norwalk Electric Works NSR Permit Application dated April 2003)
Sulfuric Acid Emission Factor from 11/27/97 CTDDEP memo
HLV values from Tables 29-1, 29-2, or 29-3 of RCSA Section 22a-174-29.
Trace organic emission factors from AP-42, Section 3.1

ATTACHMENT G

BACT DETERMINATION

ATTACHMENT G

BACT DETERMINATION

R.C.S.A. §22a-174-3a(j)(1) requires that an owner or operator shall incorporate Best Available Control Technology (“BACT”) for: potential emissions of each regulated air pollutant above the significant emission rate thresholds in Table 3a(k)-1 of §22a-174-3a(k) from each major stationary source or from each major modification; or for potential emissions of 15 tpy or more per year of any individual air pollutant from each new emissions unit or modification to each existing emission unit.

BACT for the Waterside Power Facility is a limitation on gaseous and liquid fuel such that the potential emissions of each regulated pollutant are less than the significant emission rate thresholds in Table 3a(k)-1 of §22a-174-3a(k) (see Table A-3) and the emissions from any single unit are less than 15 tpy (see Table A-2).

ATTACHMENT I

OPERATION AND MAINTENANCE PLAN

ATTACHMENT I

OPERATION AND MAINTENANCE PLAN

Installation and operation of the Waterside Project has been designed and managed to ensure maximum safety for employees and the surrounding community. All installation and operation activities and equipment for the Project have been in accordance with good engineering practice and Federal, state, and local regulations, and complies with the latest editions of the regulations of all applicable governmental agencies and engineering associations. Liquid fuel, water, and any chemicals or other hazardous materials necessary for Project operation have been appropriately contained to prevent release. In particular, liquid fuel will be stored on site in two new 126,000-gallon, double-walled storage tanks.

Safety and emergency systems have been implemented to ensure safe and reliable facility operation. The Project site is enclosed by a security fence. The Project has adopted an Emergency Action Plan. Generally, the Plan includes information on emergency operations and shutdowns, safety warning systems, emergency response personnel and duties, employee protection, training, and drills.

The Project operates in accordance with a joint Spill Prevention Control and Countermeasure/Stormwater Pollution Prevention Plan.

The Project's turbines will be operated and maintained in accordance with GE specifications such that the turbine monitoring equipment, combustion efficiency, and pollution controls will be operated so that all applicable regulations and the NSR permit will be maintained.

ATTACHMENT J

AMBIENT AIR QUALITY ANALYSIS

ATTACHMENT J

AMBIENT AIR QUALITY ANALYSIS

The only proposed change to the Waterside Power facility that could affect air quality is the replacement of the five temporary, 20,000 gals liquid fuel tanks with two 126,000 gals tanks. As shown in Attachment C, the tanks will be located in the southwest corner of the site and will each have a diameter of 40 ft and a height of 24 ft. There will be a 30 ft separation distance between the two tanks. The three TM units were remodeled adding the two tanks to the BPIP analysis (see Attachment J-1). The modeling results did not change from the previous air quality modeling analysis that was submitted to the DEP on July 21, 2006 and approved on October 4, 2006 (see Attachment J-2 and J-3).

The only changes to be made to the July, 2006 modeling results is the use of more recent DEP ambient air quality data. In July, 2006, background air quality data were only available for 2002 through 2004. Currently, data from 2005 and 2006 are now available. Thus, using the three most recent years of background data, the results are as follows.

Table J-1 presents the maximum annual average nitrogen dioxide ("NO₂") concentrations from Sherwood Island in Westport. Table J-2 presents the high second-high 1-hour and 8-hour carbon monoxide ("CO") concentrations measured at the Stamford Library.

Table J-1: Annual average NO₂ Concentrations from Sherwood Island, Westport

Year	ppm	μg/m ³
2004	0.0144	27.1
2005	0.0153	28.8
2006	0.0143	26.9

Table J-2: High Second-High 1-Hour and 8-Hour CO Concentrations from the Stamford Library

Year	1-Hour		8-Hour	
	ppm	μg/m ³	ppm	μg/m ³
2004	4	4,600.0	2.2	2,530.0
2005	3.4	3,910.0	2.5	2,875.0
2006	3.6	4,140.0	2.5	2,875.0

The highest observed concentrations are noted in bold in the above two tables. For CO, the highest modeled concentrations from the turbines are added to the observed background concentrations and compared to the NAAQS in Table J-3.

Table J-3: Comparison of Worst-Case CO Concentrations from Waterside plus Background with the NAAQS

Averaging Period	Waterside Power	Background	Total	NAAQS
	$\mu\text{g}/\text{m}^3$			
1-Hour	5,489.4	4,600.0	10,089.4	40,000
8-Hour	3,842.6	2,875.0	6,717.6	10,000

All CO concentrations are below the NAAQS using conservative modeling assumptions; thus, no further modeling analyses for CO are required.

A comparison of the worst-case annual NO₂ concentrations plus background and Pitney with the NAAQS is presented in Table 7.

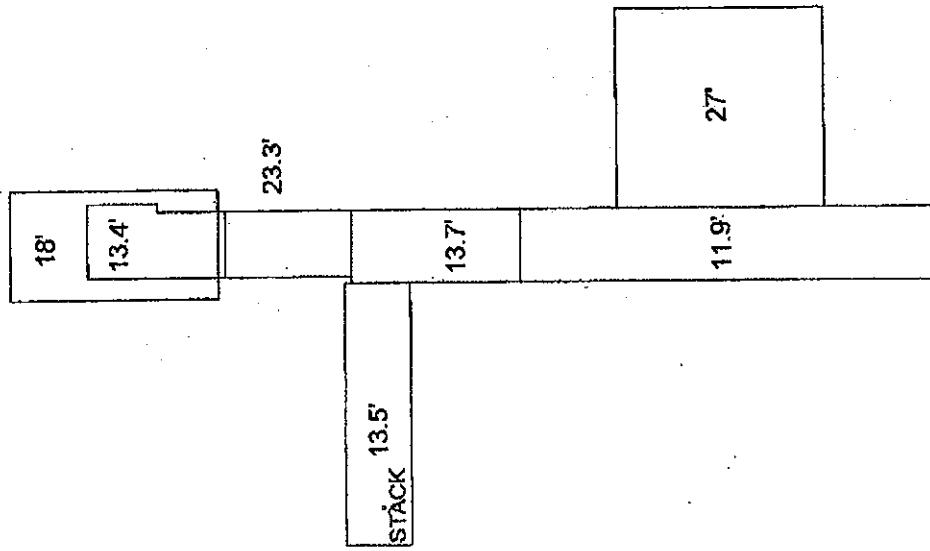
Table J-4: Comparison of Worst-Case NO₂ Concentrations from Waterside plus Pitney plus Background with the NAAQS

Averaging Period	Waterside Power	Background	Pitney	Total	NAAQS
	$\mu\text{g}/\text{m}^3$				
Annual	15.1 ¹	28.8	7.8	51.7	100

Using conservative screening modeling assumptions, the highest annual NO₂ concentration is less than the NAAQS; thus, additional modeling is not required.

¹ The July, 2006 analysis reports 15.3 $\mu\text{g}/\text{m}^3$. The current value is slightly less to take into account a decreased fuel usage (417 hours at full load versus the previous 423 hours at full load). The difference is due to the assumed heat rate of ULSD.

Schematic Building Diagram for BPIP Analysis - Waterside Power



Title One

Z:\PROJECTS\Stcwaterside\bpip.BST

Scale: 1" = 6.8 Meters

MEMORANDUM

TO: James Grillo
APCE II

FROM: Jude Catalano
APCE III

DATE: October 4, 2006

SUBJECT: Review of proposed revisions to existing facility structures Waterside Power, LLC, Stamford, Connecticut.

Waterside Power, LLC has proposed to make a few physical changes to their existing facility that would allow three existing permitted combustion turbines to operate during the winter months. The three turbines were issued permits most recently on December 2, 2005. The permit numbers are: 172-26-0228,0229 and 0230. According to a letter report I received from Blue Sky Environmental, LLC working on behalf of Waterside Power, LLC, the physical changes are to include the following:

- 1) addition of four mobile water heaters for anti-icing purposes;
- 2) the construction of turbine unit enclosures to protect the turbines from winter weather conditions;
- 3) the construction of enclosures to protect existing pumping equipment;
- 4) the installation of exhaust silencers, which will have the effect of increasing the existing stacks heights from 21 to 30 feet above grade.

The only changes from the above list that could effect existing ground-level concentrations in an adverse way would be the construction of the enclosures.

Blue Sky Environmental evaluated the downwash effects of the proposed structures with the SCREEN3 model. It was assumed that there will be no increases in the existing short term (lb/hr) or annual (tons/yr) permitted emission limits for the turbines. It was also assumed that stack operating parameters (i.e., flow rates and exit temperatures) will remain essentially the same. Results of the modeling indicate that the structural changes will not cause the source to have an adverse impact on air quality.

Please feel free to contact me if you have any questions or are faced with a different facility modification scenario.

cc: D. Wackter



BLUE SKY ENVIRONMENTAL LLC

July 21, 2006

Mr. Jude Catalano
Department of Environmental Protection
Bureau of Air Management
79 Elm Street, 5th Floor
Hartford, CT 06106-5127

Subject: **Waterside Power, LLC; Stamford
Modeling Analysis**

Dear Mr. Catalano:

As you are aware, Waterside Power, LLC ("Waterside") operates a temporary 69.2 megawatt ("MW") peaking project located in Stamford, Connecticut (the "Project"). Waterside has operated three portable General Electric TM2500 gas turbines since 2002. During the permit review process, air quality modeling analyses were reviewed by the Connecticut Department of Environmental Protection ("DEP"). The DEP has issued three individual permits for the turbines (Permit Nos. 172-26-0228 through 0230 issued most recently on December 2, 2005).

The Project wishes to participate in the ISO-NE Locational Forward Reserve Market ("LFRM") from October 1, 2006 through May 31, 2009. ISO-NE has determined that there is a need for quick-start units which can provide capacity to southwest Connecticut in the form of standby reserves beginning on October 1, 2006. Until now, the Project has only been available to operate during the summer. In order to be available year round, Waterside proposes to include the following additions to its existing equipment and operations:

- 1) addition of four (4) mobile water heaters for anti-icing protection during cold weather conditions;
- 2) use of turbine unit enclosures to protect the equipment from freezing during winter weather conditions¹;
- 3) enclosure of the two pump skids to similarly protect the existing pumping equipment;
- 4) paving of a portion of the site to allow snow clearing operations for access during the winter season;
- 5) the installation of additional exhaust silencers to ensure no adverse impacts during extended operations thereby increasing the stack height from 20.7 to 29.8 feet;
- 6) and the extension of available hours of operation from 8:00 pm to 11:00 pm.

¹ Each turbine will include two fabric enclosures: (1) 25x25x27 ft and (2) 25x13x18 ft. These enclosures affect building downwash.

The only changes listed above that could affect ground-level concentrations of pollutants are the extension of the stack height and the additional enclosures. The potential emissions associated with mobile water heaters are well below the modeling threshold. No changes are required to the individual permits since there are no hour restrictions in the permits and the stack height listed in the permit is a minimum allowable height. As per our discussions, a new screening modeling analysis has been conducted to assess the impacts associated with the proposed changes to the Project.

Modeling Methodology

Dispersion modeling was performed using the most recent version of the EPA SCREEN3 dispersion model. The SCREEN3 model was used to evaluate elevated terrain (simple, intermediate, and complex terrain). SCREEN3 was also used to determine cavity concentrations for various building structures surrounding the stack that have the potential to capture the plume in the recirculation zone.

The Good Engineering Practice (GEP) Guidelines (*Guidelines for Determination of Good Engineering Practice Stack Height, EPA-450/4-80-023R, June 1985*) provide a method for determining the GEP height for a stack based on the dimensions of the nearby structures. A structure is considered nearby if it is within "five times the lesser of the height or projected width of the structure." A "controlling" structure is that which produces the highest GEP calculated height.

The turbine stacks will be 29.8 feet above grade. The turbine generator and exhaust trains are trailer mounted in a "T" orientation. There are no existing buildings surrounding the project site which have the potential to influence the turbine stacks. The EPA BPIP program was used to evaluate the various tiers of the turbine generator housing and to calculate GEP height. A tall (27.0 feet) section of the housing is the controlling building tier for purposes of GEP. The calculated GEP height for the stacks is 67.5 feet. Since the proposed turbine stacks are less than GEP height, building downwash effects for the controlling tier were taken into consideration in the air quality modeling analysis conducted with SCREEN3. In addition to the controlling high tier section, the lower tiers of the turbine housing were also analyzed to ensure that a different building configuration did not result in a cavity entrainment scenario that leads to higher concentrations. A schematic building diagram for one unit is provided in Attachment 1.

Table 1 summarizes stack characteristics for the turbines. Table 2 provides pollutant emission rates and exhaust flow parameters for the fuel and load conditions. These operating conditions were evaluated in the modeling analysis. Based on permitted fuel usage limitations, liquid fuel-fired operation is limited to

423 hours per year (for each turbine)². Gaseous fuel-fired operation is limited to 729 hours per year (for each turbine)³. Worst-case annual impact concentrations are weighted by the maximum allowable operating hours for liquid fuel (423/8760) and gaseous fuel (729/8760) potential operating hours. The load condition for which maximum concentrations are predicted was used for comparison to the National Ambient Air Quality Standards ("NAAQS").

Table 1: Stack Characteristics for the Proposed Project

Base Elevation, msl (feet/meters)	54.5 / 16.6
Stack Height (feet/meters)	29.8 / 9.083
Equivalent Inside Stack Diameter (feet/meters)	9.28 / 2.83
Number of Stacks	3
Predominate Land Use Type	Urban
Stack 1 Location:	
UTM-E (m)	621,315.1
UTM-N (m)	4,543,660.6
Stack 2 Location:	
UTM-E (m)	621,293.9
UTM-N (m)	4,543,647.9
Stack 3 Location:	
UTM-E (m)	621,268.0
UTM-N (m)	4,543,634.7

² The NSR permits limit the total fuel usage from the TM2500 units to 2,285,322 gallons per consecutive 12 months. Based on a maximum fuel firing rate of 1,800 gal/hr, this equates to 1269.6 hours total or 423 hours per turbine.

³ The NSR permits limit the total fuel usage from the TM2500 units to 549,257,047 scf per consecutive 12 months. Based on a maximum fuel firing rate of 251,000 scf/hr, the maximum permitted, this equates to 2,188.3 hours total or 729.4 hours per turbine.

Table 2: Stack Parameters for the Waterside Power Turbines (per Turbine)

Fuel	Liquid Fuel			Liquid Fuel			Gaseous Fuel			
	100%	100%	100%	100%	100%	100%	100%	100%	100%	
Load										
Ambient Temperature	°F	90	90	90	0	50	100	0	50	100
Exit Temperature	°K	827.44	813.00	802.44	741.33	788.56	808.56	737.44	787.44	805.22
Exit Velocity	m/s	26.04	25.15	24.33	25.40	25.65	23.23	25.50	25.92	23.78
NO _x	g/s	5.11	4.84	4.62	5.04	5.04	4.28	2.90	2.93	2.53
CO	g/s	1.19	1.40	1.60	6.66	3.22	1.30	7.00	3.78	1.24

The SCREEN3 model was used to predict maximum 1-hour ground level pollutant concentrations. Maximum 1-hour impacts for simple terrain were converted to other averaging periods using the recommended scaling factors shown below.

$$\text{8-hour avg.} = 0.7 \times \text{1-hour avg.}$$

$$\text{Annual-hour avg.} = 0.08 \times \text{1-hour avg.}$$

For complex terrain, the following recommended scaling factors were used:

$$\text{8-hour avg.} = 2.8 \times \text{24-hour avg.}$$

$$\text{Annual-hour avg.} = 0.32 \times \text{24-hour avg.}$$

Receptors for the screening analysis were located at 34 meters (just outside the property fenceline), and then at 25-meter intervals from 50 to 100 meters, at 50-meter intervals from 100 to 200 meters, at 100-meter intervals from 200 to 2,000 meters, at 200-meter intervals from 2,000 to 4,000 meters, at 500-meter intervals from 4,000 to 5,000 meters, and at 1,000-meter intervals from 5,000 to 10,000 meters. Discrete elevated receptors up to the VALLEY (stable) plume height were also input to the model for evaluation of complex terrain. Receptor elevations were selected based on the highest elevation found within a sector defined by the midpoint distances between adjacent receptors. The receptor elevations were selected based on the highest elevation at given distances from the proposed source location, regardless of direction.

One-hour worst-case concentrations for simple terrain, 24-hour worst-case concentrations for complex terrain, and 1-hour worst-case cavity concentrations, were determined for unit emissions (1.0 g/s). These concentrations were then scaled by the NO_x and CO emission rates and appropriate time averaging factors.

Cavity Analysis

Since emissions from the turbines will be released from a stack that is less than GEP height, the potential for emissions being entrained into the recirculation zone (cavity) was considered. The cavity analysis was conducted using the SCREEN3 model that provides the length of the cavity and recirculation zone concentrations for non-GEP stacks. Separate building tiers were evaluated. SCREEN3 results indicate that the turbine plumes will either (1) NOT be entrained in building cavities, or (2) have a cavity length that will NOT go beyond the facility property fenceline. Therefore, cavity concentrations will not impact ambient air quality.

SCREEN3 Model Results and Impact Analysis

The worst-case impacts for the combustion turbines were found to occur just outside the property line (a simple terrain receptor) at an ambient temperature of 0°F. Maximum predicted impact concentrations are provided in Table 3.

Table 3: Maximum Predicted SCREEN3 Concentrations

Pollutant	Averaging Period	Maximum Concentrations ($\mu\text{g}/\text{m}^3$)	Maximum Impact Case
NO ₂	Annual	15.3	Liquid Fuel, 100% Load, 0°F
CO	1-Hour	5,489.4	Gaseous Fuel, 100% Load, 0°F
CO	8-Hour	3,842.6	Gaseous Fuel, 100% Load, 0°F

The closest representative DEP background monitor for NO₂ is on Sherwood Island in Westport and the closest CO monitor is at the Stamford Library at 96 Broad Street.

Table 4: Annual average NO₂ Concentrations from Sherwood Island, Westport

Year	ppm	$\mu\text{g}/\text{m}^3$
2004	0.0144	27.1
2003	0.0164	30.8
2002	0.0187	35.2

Table 5: High Second-High 1-Hour and 8-Hour CO Concentrations from the Stamford Library

Year	1-Hour		8-Hour	
	ppm	$\mu\text{g}/\text{m}^3$	ppm	$\mu\text{g}/\text{m}^3$
2004	4	4,600.0	2.2	2,530.0
2003	3.8	4,370.0	2.6	2,990.0
2002	4.4	5,060.0	3.2	3,680.0

The highest observed concentrations for both NO₂ and CO were observed in 2002. For CO, the highest modeled concentrations from the turbines are added to the observed background concentrations and compared to the NAAQS in Table 6.

Table 6: Comparison of Worst-Case CO Concentrations from Waterside plus Background with the NAAQS

Averaging Period	Waterside Power	Background	Total	NAAQS
	$\mu\text{g}/\text{m}^3$			
1-Hour	5,489.4	5,060.0	10,549.4	40,000
8-Hour	3,842.6	3,680.0	7,522.6	10,000

All CO concentrations are below the NAAQS using conservative modeling assumptions; thus, no further modeling analyses for CO are required.

For NO₂, as per your recommendation, all sources within the significant impact level ("SIL") were modeled. The annual averaged SIL for NO₂ is 1 $\mu\text{g}/\text{m}^3$. The screening modeling shows that the SIL for NO₂ is modeled between 200 and 300 m from the Waterside stacks using worst-case modeling results. Thus, for conservativeness, all sources within 300 m (or 984 ft) were modeled. Figure 1 shows a 300 m radius around Waterside Power (highlighted in yellow) with various land use categories identified. The types of facilities (industry, office, golf courses, residences, etc.) found within these land uses are summarized in Attachment 2. A detailed review of the DEP record files along with a field site review indicated that there is only one source within 300 m of Waterside Power that is permitted by the DEP as an air emission source. The DEP's Point Source Emissions Inventory for Stamford (see Attachment 3) indicates that Pitney Bowes ("Pitney") located at 23 Barry Place in Stamford (Premise Number 172) operates one permitted source, a 250 hp boiler (Permit No. 172-002). This boiler was installed in 1972. The inventory also indicates that there is a grandfathered 400 hp boiler at the site installed in 1967 and an emergency generator installed in 1972. Correspondence with Pitney indicates that the emergency generator has been removed from the site.

The 250-hp boiler was originally modeled by you in 1979 (see Attachment 4). The stack parameters used in that modeling analysis were used to model Pitney with SCREEN3 for this analysis at the same receptors that were modeled for Waterside. The modeling conservatively used the lower of the ACFM for Pitney. The approximate distance from Pitney to Waterside is 200 m. The maximum NO₂ impact from Waterside is found at 34 m. The distance from Pitney to the distance of the maximum NO₂

Mr. Jude Catalano
Department of Environmental Protection
July 21, 2006

Page 7

concentration modeled for Waterside is 166 m (or 200 m – 34 m). Conservatively, the higher concentration modeled for Pitney for receptors at 150 and 200 m were used to approximate the concentration at 166 m. The highest 1-hour concentration of 97.69 $\mu\text{g}/\text{m}^3$ for Pitney was found at 150 m. Converting this to an annual impact by scaling by 0.08 results in annual concentration of 7.8 $\mu\text{g}/\text{m}^3$. A comparison of the worst-case annual NO_2 concentrations plus background and Pitney with the NAAQS is presented in Table 7.

Table 7: Comparison of Worst-Case NO_2 Concentrations from Waterside plus Pitney plus Background with the NAAQS

Averaging Period	Waterside	Background	Pitney	Total	NAAQS
	Power			$\mu\text{g}/\text{m}^3$	
Annual	15.3	35.2	7.8	58.3	100

Using conservative screening modeling assumptions, the highest annual NO_2 concentration is less than the NAAQS; thus, additional modeling is not required.

This analysis is based on the current winterization design of the facility. If the final design changes the air modeling results, an update will be submitted to you. If you require additional information or have any questions, please do not hesitate to call me at 617-834-8408.

Sincerely,
Blue Sky Environmental LLC



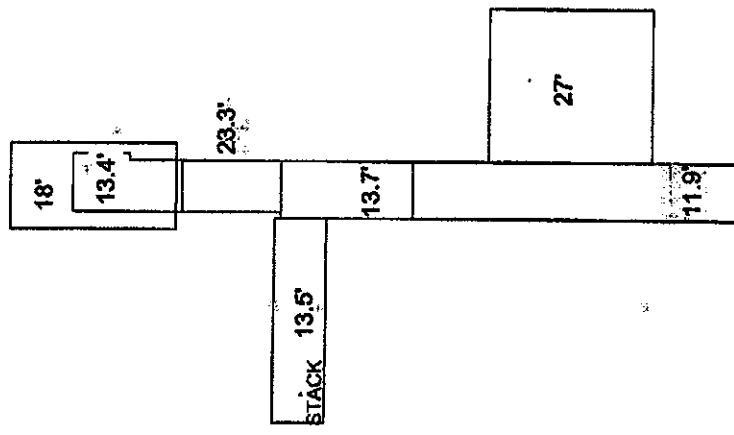
Donald C. DiCristofaro, CCM
President

Attachments

Cc: J. Grillo, DEP
T. Atkins, Waterside Power

Attachment 1. Schematic Building Diagram for one TM2500 Unit

Schematic Building Diagram for BPIP Analysis-Waterside Power



ZAPROJECTS\hwaterside\bip.BST
Waterside Power, Stamford, CT

Scale: 1" = 7.9 Meters

EARTH TECH

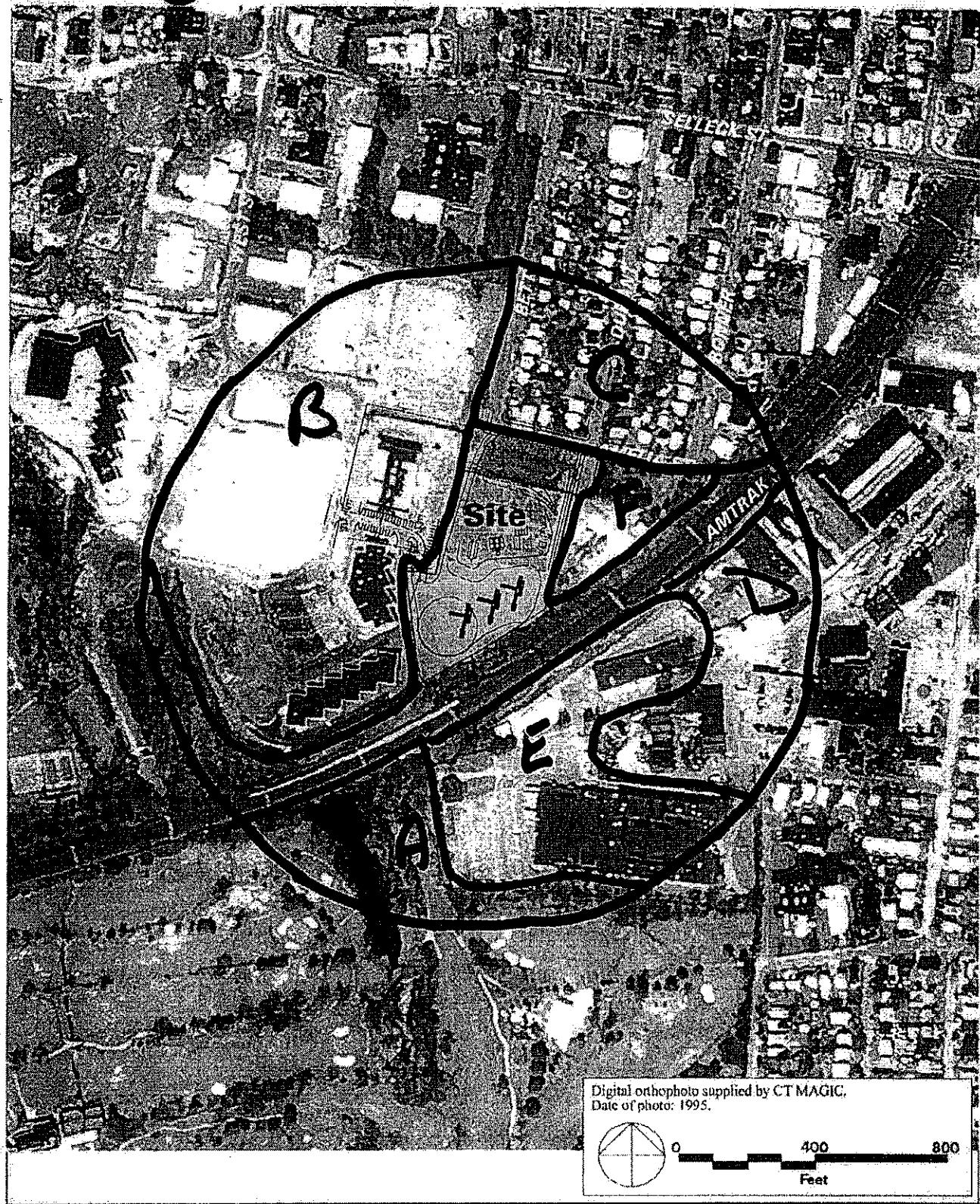


Figure 1. Land use within 300 m surrounding Waterside Power.

ATTACHMENT 2

Facilities Around Waterside Power

A

Innis Arden Golf Club

B

US Postal Service

404 and 420 West Avenue
Goodway

470 West Avenue
Corporate Branching LLC
Kirby Lester LLC
Jofemer USA
Columbus IT Partners
Fugazy Travel
Corebrand
Staples
Morrow and Co.
First Presbyterian Church of Greenwich

550 West Avenue
Davidoff of Geneva
Performance Imaging
Tepnel Litecodes

600 West Avenue
FedEx

650 West Avenue
Davidoff of Geneva

Fuji Film

The Iron Shop – Spiral Stair Kits
Broad Reach Partners, Business Development Specialists

C

Residential

60 Bonner
Arcadia

D

375 Fairfield Avenue
Creative Cabinetry
Stamford Wrecking Co.
Connaught - Gum Busters
Landmark Document Services
Connecticut Floor Supply
Flower Beauty Products
Ionian Food Imports
Jack Rabbit Energy Systems
The Packaging Store
All Marine Spares International
Ideal Stonework
Jonathan Podmore Cabinetry
NY-CT Development Corp.
Jacobson Woodworking

35 Melrose Place
Mosaic True Blue

One Barry Place
USPS Barry Place Annex
English Country Garden
John Deere Landscape
E.T. Warehouse
Connecticut Floor Store
Contemporary Lighting
Scotts Lawn Services

E

23 Barry Place
Pitney Bowes

F

CL&P Substation

Attachment 3. DEP Point Source Emissions Inventory for Stamford

SAS

**CONN BUREAU OF AIR MANAGEMENT
2004 POINT SOURCE EMISSIONS INVENTORY BY TNN PREM STACK REG**

15:49 Wednesday, July 27, 2005 100

CLI	TNN	PRSM	STK	P	RSG	Date Shutdown	C	Date Startup	Equipment Description	Proc SCC	SCC #1	Company Name	SIC	Data Year	
5643	171	1	16	R	36	P	01/01/1968		CURE OVEN & IMPREGNATOR	40201301	390001089	CUNO INC	3569	1997	
5643	171	1	17	R	37	P	01/01/1954		GRINDER #1S	39999999	00000000	CUNO INC	3569	1997	
5643	171	1	18	R	38	P	01/01/1968		GRINDER #2N	39999999	00000000	CUNO INC	3569	1997	
5643	171	1	802	U	2	P	01/01/1989		PAPER COATING	40201301	00000000	CUNO INC	3569	1997	
1984	171	2	2	R	65	P	11/01/1963		BLR O&S 100	00000000	10200501	COOLEY CO., B P	2231	1990	
6383	171	5	1	R	4	P	01/01/1963		BLR ERIE CITY WT	00000000	10200504	FIORE-WITTENZELLNER-PIS	6512	1990	
1991	171	9	1	P	20	P	07/01/1982		BLR CB 800-150	00000000	10200504	TYCO PRINTED CIRCUIT GR	3679	1996	
1991	171	9	1	P	26	P	08/28/1989		BLR BURNHAM 3P-150-4	00000000	10200504	TYCO PRINTED CIRCUIT GR	3679	1996	
1991	171	9	801	U	1	P	10/01/1991		THINNING SOLVENTS: MEK	40200918	00000000	TYCO PRINTED CIRCUIT GR	3679	1996	
6046	171	10	5	S	1	P	10/01/1991		ALBA DRYER	00000000	10500110	WARREN CORP	2231	1996	
6046	171	10	4	P	15	P	07/12/1976		BLR CB 655-500	#1	00000000	10200501	WARREN CORP	2231	1996
6046	171	10	4	P	23	P	BLR CB 655-500	#4	00000000	10200501	WARREN CORP	2231	1996		
6046	171	10	1	R	13	P	08/26/1964		BLR CB 655-350	#1	00000000	10200401	WARREN CORP	2231	1996
6046	171	10	2	R	14	P	08/26/1964		BLR CB 655-350	#2	00000000	10200401	WARREN CORP	2231	1996
6046	171	10	3	R	15	P	09/29/1970		BLR CB 655-350	#3	00000000	10200401	WARREN CORP	2231	1996
1993	171	12	1	R	51	P	SAND & GRAVEL HOPPER		30501108	00000000	MOTTES CO., J J	3273	1979		
5821	171	15	1	P	42	P	CLEAR POLISHING CO., VFW		30999999	00000000	WILLINGTON NAMEPLATE IN	3479	5555		
5821	171	15	801	U	1	P	MISC METAL PARTS: COATI		40202501	00000000	WILLINGTON NAMEPLATE IN	3479	1994		
5590	171	28	801	U	1	P	WOOD FURNITURE COATING		40201901	00000000	BUCH'S ANTIQUE SHOP	7641	1989		
1996	171	35	2	P	14	P	BLRS CB 600-300 (2)		00000000	10300501	JOHNSON MEMORIAL HOSPIT	8062	1996		
1996	171	35	3	P	22	P	ELECT MACH 7250IT DIESEL		00000000	20300101	JOHNSON MEMORIAL HOSPIT	8062	1996		
1999	171	43	1	R	71	P	BLR KEWANEE	#1	00000000	10300501	STAFFORD HIGH SCHOOL	8211	1990		
1999	171	43	1	R	72	P	BLR KEWANEE	#2	00000000	10300501	STAFFORD HIGH SCHOOL	8211	1990		
1999	171	44	1	R	73	P	BLR HB SMITH 44-17	#1	00000000	10300501	WITT MIDDLE SCHOOL, E	8211	1990		
1999	171	44	1	R	74	P	BLR HB SMITH 44-17	#2	00000000	10300501	WITT MIDDLE SCHOOL, E	8211	1990		
7811	171	50	1	P	29	P	KOHLER 35HZ DIESEL		00000000	20301001	CELILCO PARTNERSHIP	4813	5555		
2002	172	3	1	R	4	P	60" EGAN PAPER CENTER		40201301	39000689	GAISSE INC., E J	2796	1991		
2004	172	3	6	R	447	P	22" EXPT WEB COATER		40201301	39000689	GAISSE INC., E J	2796	1991		
2004	172	5	1	R	7	P	BLR I.B.W. CR355		00000000	10200501	TODD COMBUSTION INC	3599	1990		
2004	172	5	801	U	1	P	OPEN-TOP VAPOR DEGREASI		40209205	00000000	TODD COMBUSTION INC	3599	1976		
2004	172	5	802	U	2	P	SPRAY BOOTH		40209396	00000000	TODD COMBUSTION INC	3599	1976		
2006	172	6	1	R	8	P	BLR 100HP ???		00000000	10200504	FIRST STAMFORD CORP	6512	1983		
2006	172	7	1	R	9	P	BLR PETRO PAC 301W125		00000000	10300501	KING LOW HEYWOOD THOMAS	8299	1990		
2008	172	8	1	R	10	P	BLR BIGELOW FT		00000000	10200504	TERMATOOL CORP	3548	1987		
1138	172	10	1	R	13	P	B10/01/1954		00000000	-10300504	UNIV OF CT / STAMFORD	8221	1990		
1138	172	10	1	R	13	P	BLR FITZGIBBONS #1		00000000	-10300504	UNIV OF CT / STAMFORD	8221	1990		
2011	172	12	1	R	16	P	09/28/1967		00000000	10300504	HEYMAN ASSOC #1	6512	1997		
2011	172	12	1	R	17	P	09/28/1967		00000000	10300504	HEYMAN ASSOC #1	6512	1997		
2011	172	12	1	R	18	P	09/28/1967		00000000	10300504	HEYMAN ASSOC #1	6512	1997		
6565	172	17	6	P	48	P	REACTOR PIPERACTM IN PR		30106099	00000000	CYTC INDUSTRIES INC	8731	5555		
6565	172	17	7	P	66	P	11/01/1995		49099999	00000000	CYTC INDUSTRIES INC	8731	1996		
6565	172	17	3	R	43	P	B01/01/1950		BLR BIGELOW B 25K# / H #4	00000000	10200401	CYTC INDUSTRIES INC	8731	1996	
6565	172	17	3	R	44	P	B01/01/1958		BLR BIGELOW HT88 50K# / H	00000000	10200401	CYTC INDUSTRIES INC	8731	1996	
6565	172	17	5	R	486	P	01/01/1970		MIXING KETTLE (4 UNITS)	30199999	00000000	CYTC INDUSTRIES INC	8731	1996	
7738	172	23	1	P	56	P	01/01/1970		REACTORS (12 UNITS)	30199999	00000000	CYTC INDUSTRIES INC	8731	1996	
7738	172	23	1	P	179	P	BLR FEDERAL FEP200		00000000	10300504	CSC 65 PROSPECT STREET	6513	1994		
7050	172	24	1	P	164	P	FEDERAL 8.4 MBTU BOILERS		00000000	10300501	CSC 65 PROSPECT STREET	6513	5555		
8048	172	26	1	P	1	P	09/23/2004	C	1250KW BLACK START GEN	00000000	10300501	COHN BIRNBAM PC	6512	5555	
8048	172	26	1	P					WATERSIDE POWER LLC	00000000		WATERSIDE POWER LLC	4911	2004	

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